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Study of Performance of Shaft output with Rotor-to-Casing Ratios versus Different Vane Angles Adopting Practical Approach on a Novel Multi-Vane Air Turbine

By Bharat Raj Singh , Onkar Singh

SMS Institute of Technology, Gosainganj, Lucknow, UP, India

Abstract - A concept of using compressed atmospheric air as an alternative to fossil fuel and zero pollution power sources for running light vehicle such as: motorbikes etc.. Here considered vehicle is equipped with an air turbine in place of an internal combustion engine, and transforms the compressed air energy into shaft work. The mathematical modeling shown here is reproduced from author's earlier publications on a small capacity compressed air driven vaned type novel air turbine. The effect of different rotor to casing diameter ratios with respect to different vane angles (number of vanes) have been considered and analyzed under specific parametric conditions. The shaft work output is found optimum adopting practical conditions of rotor / casing diameter ratios on a particular value of vane angle (no. of vanes). In this study, the maximum power is obtained as 4.02 kW (5.6 HP) when casing diameter is taken 100 mm, and rotor to casing diameter ratio is kept from 0.70, as the construction of turbine can be fabricated between rotor to casing (d/D) ratio from 0.95 to 0.70 only. It is learnt that the generated power output of 4.02 kW (5.6 HP) is sufficient to run any motorbike.

Keywords : zero pollution, compressed air, air turbine, vane angle, rotor / casing diameter ratio, air-o-cycle.

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Study of Performance of Shaft output with Rotor-to-Casing Ratios versus Different Vane Angles Adopting Practical Approach on a Novel Multi-Vane Air Turbine

Bharat Raj Singh^a, Onkar Singh^Q

Abstract - This paper describes a concept of using compressed atmospheric air as an alternative to fossil fuel and zero pollution power sources for running light vehicle such as: motorbikes etc.. Here considered vehicle is equipped with an air turbine in place of an internal combustion engine, and transforms the compressed air energy into shaft work. The mathematical modeling shown here is reproduced from author's earlier publications on a small capacity compressed air driven vane type novel air turbine. The effect of different rotor to casing diameter ratios with respect to different vane angles (number of vanes) have been considered and analyzed under specific parametric conditions. The shaft work output is found optimum adopting practical conditions of rotor / casing diameter ratios on a particular value of vane angle (no. of vanes). In this study, the maximum power is obtained as 4.02 kW (5.6 HP) when casing diameter is taken 100 mm, and rotor to casing diameter ratio is kept from 0.70, as the construction of turbine can be fabricated between rotor to casing (d/D) ratio from 0.95 to 0.70 only. It is learnt that the generated power output of 4.02 kW (5.6 HP) is sufficient to run any motorbike.

Keywords : zero pollution, compressed air, air turbine, vane angle, rotor / casing diameter ratio, air-o-cycle.

I. INTRODUCTION

It is an established fact that the Worldwide faster consumptions of fossil fuel in transport vehicles have resulted fast depletion to energy resources and releasing huge quantities of pollutant in the atmosphere.. A US geologist Marian King Hubbert [1] in 1956 indicated that the conventional crude-oil production will attain Peak Oil within 20 years and thereafter it will start depleting which may cause serious threat to mankind within 40 years i.e. by 1995. Aleklett K. and Campbell C.J., [2] in 2003 illustrated that with current rate of consumptions, the production of oil and gas in many country will peak and begin to decline by around 2010. Such apprehension has led the search for environment friendly alternative to fossil fuel oil, or some

method of conserving natural resources using non-conventional options, such as; biodiesel, wind power, photo voltaic cells etc. and or energy conversion systems like battery storage, hydrogen cell, compressed air etc to obtain shaft work for the engines of vehicles [3-9].

Guy Negre [10] a French technologist and G. Saint Hillarie [11] an inventor of quasi turbine have carried out very important work in the area of compressed air engine. They stored highly compressed air in the energy storage systems up to 300 bar pressure within 15-20 minutes, and reused for running compressed air engines. In view of such attractive features of nearly zero pollution and air compression by using non-conventional resources, the compressed air engine became comparable in place of the other technology in vehicle markets.

In this paper author has carried out the parametric analysis of a small capacity air turbine having vane type rotor and describes the investigation of the effect of rotor to casing diameter ratios with different vanes fitted in the rotor. Results obtained by using a mathematical model are presented and analyzed here.

II. FEATURE OF VANE TYPE AIR TURBINE

In this study a multi-vane type air turbine having casing diameter =D mm and rotor diameter =d mm is proposed as shown in Fig. 1. The considered air turbine works on the reverse working principle of vane type compressor. In this arrangement total shaft work is seen to be the cumulative effect of isobaric admission of compressed air jet on vanes and the adiabatic expansion of high pressure air. In earlier study conducted by authors a prototype of air turbine was developed [12].and its functionality was examined. A storage cylinder for the compressed air having capacity of 30 minutes stored air, for the requirement of running turbine at initial stage at working pressure of 10 bar, is used as a compressed air energy source. This storage cylinder is designed to produce constant pressure for the minimum variation of torque at low volumes of compressed air and attached with filter, regulator and lubricator. The clean air then admits into air turbine

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through its inlet nozzle and vanes of air turbine are also fitted into rotor under spring loading to maintain their regular contact with the casing wall. This arrangement is proposed to minimize leakage through mating contacts and is novelty of improvement in the vane turbine. A study on highly efficient energy conversion system for liquid nitrogen [13], design and verification of airfoil and its tests, influence of tip speed ratios for small wind turbine and parabolic heat transfer and structural analysis were also carried out for conceptualizing the energy conversion system [14-17]. The study of design feasibility of vane type novel air turbine has also been carried out [18-21].

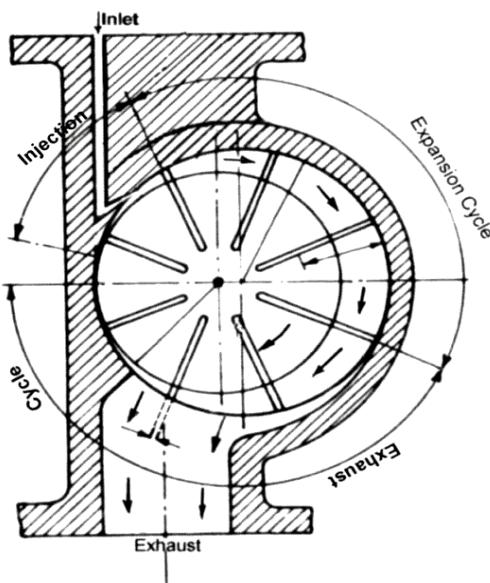


Fig.1 : Air Turbine-Model

The present objective of this study is to investigate the power output of an air turbine with different number of vanes in rotor, i.e. angle between first two consecutive vanes and the rotor/casing ratio (d/D). The air turbine considered has capability to yield output of 5.0 to 5.6 HP at injection pressure 4-6 bar and speed of 2000-2500 rpm and is suitable to run a motorbike.

III. MATHEMATICAL MODEL

The mathematical model shown here is already presented in author's earlier publications [22-34] and is reproduced here for maintaining the continuity and benefits to the readers**1. The high pressure jet of air at ambient temperature drives the rotor in novel air turbine due to both isobaric admission and adiabatic expansion. The high pressure air when enters through the inlet passage, pushes the vane for producing rotational movement and thereafter air so collected

between two consecutive vanes of the rotor is gradually expanded up to exit passage, also contributes to the shaft out. This isobaric admission and adiabatic expansion of high pressure air both produces the total shaft power output from air turbine. Compressed air leaving the air turbine after expansion is sent out from the exit passage. It is thus noticed that the scavenging of the rotor is perfect and the work involved in recompression of the residual air is absent as seen from Fig. 1.

From Fig. 2, it is seen that work output is due to isobaric admission (E to 1), and adiabatic expansion (1 to 4) and reference 2, 3 in the figure shows the intermediate position of vanes. Thus, total work output due to thermodynamic process may be written as:

$$\text{Total work output} = [\text{Thermodynamic expansion work } (w_1)] + [\text{Exit steady flow work } (w_2)]$$

or

$$w = [(w_1) + (w_2)] \quad (1)$$

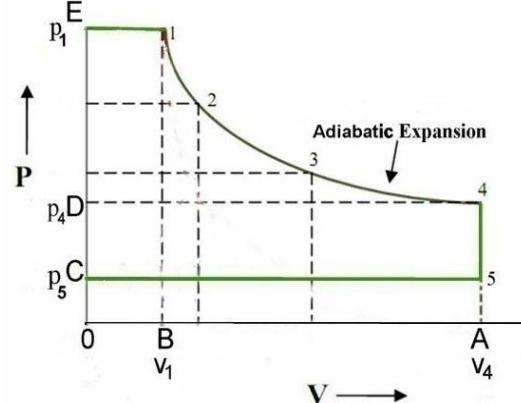


Fig.2 : Thermodynamic Processes (Isobaric, adiabatic and Isochoric Expansion)

Now thermodynamic expansion work (w_1), considering adiabatic process between state 1 and 4, it can be written as:

$$w_1 = \left(\frac{\gamma}{\gamma-1} \right) \cdot p_1 \cdot v_1 \cdot \left\{ 1 - \left(\frac{p_4}{p_1} \right)^{\frac{\gamma-1}{\gamma}} \right\} \quad (2)$$

The process of exit flow (4-5) takes place after the expansion process (E-4) as shown in Fig. 2 and air is released to the atmosphere. In this process; till no over expansion takes place pressure p_4 can't fall below atmospheric pressure p_5 . Thus at constant volume when pressure p_4 drops to exit pressure p_5 , no physical work is seen. Since turbine is functioning as positive displacement machine and hence under steady fluid flow at the exit of the turbine, the potential work is absorbed by the rotor and flow work (w_2), can be written as:

**1 Mathematical model is reproduced here from author's earlier publications [22-34].

$$w_2 = \int_4^5 v.dp = v_4(p_4 - p_5) \quad (3)$$

Applying equations (2), (3) into equation (1), considering air turbine has n number of vanes, then shaft output [35] can be written as:

$$w_n = n \left(\frac{\gamma}{\gamma-1} \right) \cdot p_1 \cdot v_1 \left\{ 1 - \left(\frac{p_4}{p_1} \right)^{\frac{\gamma-1}{\gamma}} \right\} + n \cdot (p_4 - p_5) \cdot v_4 \quad (4)$$

where w_n is work output (in Nm), for complete one cycle.

Therefore, the total power output or work done per unit time (W), for speed of rotation N rpm, will be:

$$W_{total} = n \cdot (N/60) \cdot \left(\frac{\gamma}{\gamma-1} \right) \cdot p_1 \cdot v_1 \left\{ 1 - \left(\frac{p_4}{p_1} \right)^{\frac{\gamma-1}{\gamma}} \right\} + n \cdot (N/60) \cdot (p_4 - p_5) \cdot v_4 \quad (5)$$

Figure 1 shows that if vanes are at angular spacing of θ degree, then total number of vanes will be $n = (360/\theta)$. The variation in volume during expansion from inlet to exit (i.e. v_1 to v_4) can be derived by the variable extended length of vane as shown in Fig. 3 at every point of movement between two consecutive vanes.

From Fig. 3, shows that when two consecutive vanes at OK and OL move to position OH and OB, the extended vane lengths varies from SK to IH and LM to BG, thus the variable length BG at variable α_i is assumed as $X_{at\ variable\ \alpha}$ can be written from the geometry:

$$BG = x_{at\ variable\ \alpha} = R \cdot \cos \left[\sin^{-1} \left\{ \left(\frac{R-r}{R} \right) \cdot \sin \alpha \right\} \right] + (R-r) \cdot \cos \alpha - r \quad (6)$$

where $2R=D$ is diameter of casing and $2r=d$ is diameter of rotor, α is angle $\angle BOF$, β is angle $\angle BAF$ and θ is angle $\angle HOB$ or $\angle H'OB$ or $\angle KOL$, between two consecutive vanes and ϕ is angle $\angle KOJ$ at which injection pressure admits to the air turbine.

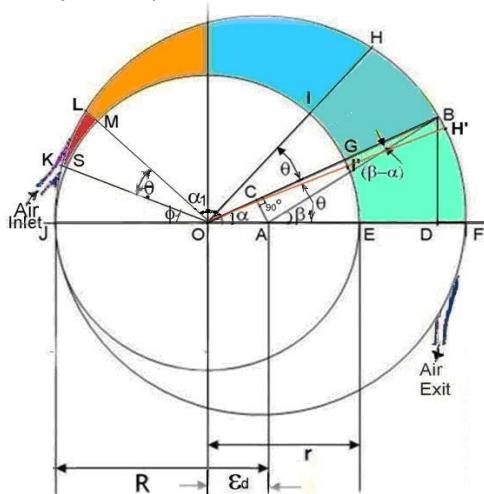


Fig.3 : Variable length BG and IH and injection angle θ

Variable volume of cuboids B-G-I-H-B can be written as:

$$v_{cuboids} = L \cdot \left\{ \frac{(X_{1i} + X_{2i})(2r + X_{1i})}{4} \right\} \cdot \sin \theta \quad (7)$$

where $BG = X_{1i}$ and $IH = X_{2i}$ variable length of vanes when rotate into turbine as shown in Fig. 3 and i stands for min or max length. Thus

a) The volume at inlet v_1 or v_{min} will fall between angle $\angle LOF = \alpha_{1min} = (180 - \theta - \phi)$ and angle $\angle KOF = \alpha_{2min} = (\alpha_{1min} + \theta) = (180 - \phi)$ as seen in Fig. 3, when air is admits into turbine at angle ϕ .

b) The Volume at exit v_4 or v_{max} will fall between angle $\angle BOF = \alpha_{1max} = \alpha = 0$ and angle $\angle HOF = \alpha_{2max} = (\alpha_{1max} + \theta) = \theta$.

Applying above conditions into equations (6), then $LM = X_{1min}$, $SK = X_{2min}$, $FE = X_{1max}$ =Corresponding to BG at $\alpha = 0$ degree and $I'H' = X_{2max}$ =Corresponding IH at $(\alpha + \theta) = \theta$ degree

Applying values of X_{1min} and X_{2min} to equation (7),

$$v_{min} = v_1 = L \cdot \left\{ \frac{(X_{1min} + X_{2min})(2r + X_{1min})}{4} \right\} \cdot \sin \theta \quad (8)$$

Applying values of X_{1max} and X_{2max} to equation (7),

$$v_{max} = v_4 = L \cdot \left\{ \frac{(X_{1max} + X_{2max})(2r + X_{1max})}{4} \right\} \cdot \sin \theta \quad (9)$$

Applying values of v_1 and v_4 from equations (8) and (9) to equation (5), the total power output available W_{total} can be written as :

$$W_{total} = n \cdot (N/60) \cdot \left(\frac{\gamma}{\gamma-1} \right) \cdot \left\{ 1 - \left(\frac{p_4}{p_1} \right)^{\frac{\gamma-1}{\gamma}} \right\} \cdot p_1 \cdot \left[L \cdot \left\{ \frac{(X_{1min} + X_{2min})(2r + X_{1min})}{4} \right\} \cdot \sin \theta \right] + n \cdot (N/60) \cdot (p_4 - p_5) \cdot \left[L \cdot \left\{ \frac{(X_{1max} + X_{2max})(2r + X_{1max})}{4} \right\} \cdot \sin \theta \right] \quad (10)$$

IV. PARAMETRIC CONSIDERATIONS AND ANALYSIS

In this study various input parameters are listed in Table 1 for investigation of performance of vane turbine at different rotor to casing diameter ratios (d/D) with respect to different vane angle when $D=100$ mm, injection pressure 6 bar (90 psi) and its optimization for larger shaft output.

Table 1 : Input Parameters

Symbols	Parameters
d/D Ratio	0.95, 0.9, 0.85, 0.80, 0.75 and 0.70 when casing diameter is kept $D=100$ mm
p_1	6 bar (≈ 90 psi) – inlet pressures
p_5	$(p_4 / 1.2) > 1.0132$ bar (atmospheric pressure)
p_4	$(v_1 / v_4)^{\gamma} \cdot p_1 > p_5$ assuming adiabatic expansion
N	2500 rpm (as total power is directly proportion to rpm)
L	45 mm length of rotor (assumed minimum)
γ	1.4 for air
n	Number of vanes in the rotor = $(360 / \theta)$
θ	Vane angle = 30° (12 vanes), 36° (10 vanes), 45° (8 vanes), 60° (6 vanes), and 90° (4 vanes)
ϕ	60° angle at which compressed air enters through nozzle into rotor

While actual fabrication of air turbine is carried out, it is noticed that the rotor / casing (d/D) ratio can possibly be varied from 0.95 to 0.70 only.

V. RESULTS AND DISCUSSION

Based on the various input parameters listed in Table-1 and mathematical model, the effects of different rotor to casing diameters ratios, at different vane angles, 2500 rpm of speed of rotation and 6 bar of injection pressure on the expansion work, exit flow work and total work output from air turbine are studied. Here the injection angle (ϕ) of the air turbine is considered to be constant at 60° for whole study.

The results obtained have been plotted in Figs. 4 to 9, for the rotor to casing diameter ratio (d/D), varied as 0.95, 0.90, 0.85, 0.80, 0.75 and 0.70 at different vanes of rotor 12, 10, 8, 6, 4 (i.e. corresponding vanes angles of 30° , 36° , 45° , 60° , 90°) and injection angle of 60° at injection pressures of 90 psi and at the speed of rotation 2500 rpm.

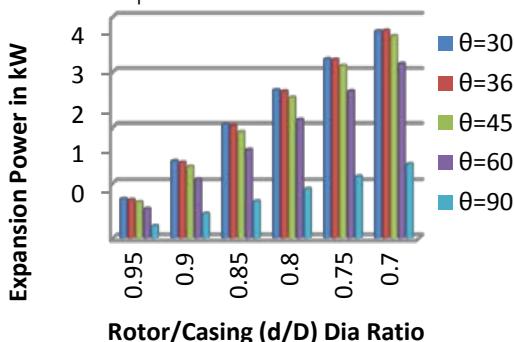


Fig.4 : Expansion power versus rotor / casing diameter (d/D) ratio at different rotor vanes when $D= 100$ mm, injection pressure = 6 bar and speed of rotation = 2500 rpm.

Figure 4 shows the variation of expansion power for the rotor vanes = 12 nos. ($\theta=30^\circ$), 10 nos.

($\theta= 36^\circ$), 8 nos. ($\theta= 45^\circ$), are increasing linearly at rotor / casing ratios = 0.95, 0.90, 0.85, 0.80, 0.75 to 0.70 and it almost varies in similar values. Thus optimal performance of expansion power is seen at rotor / casing ratios = 0.70 for vanes number 12 to 8. But variation of expansion power for the rotor vanes = 6 nos. ($\theta=60^\circ$), and 4 nos. ($\theta= 90^\circ$), are increasing almost linearly at rotor / casing ratios = 0.95, 0.90, 0.85, 0.80, 0.75 & 0.70 and developed power values are smaller.

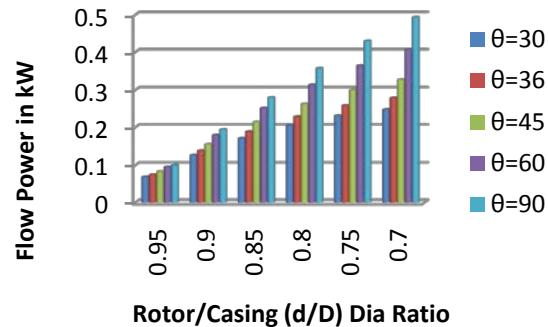


Fig.5 : Exit flow power versus rotor / casing diameter (d/D) ratio at different vane number (vane angles) when $D=100$ mm, injection pressure = 6 bar and speed of rotation = 2500 rpm.

Figure 5 shows the variation of flow power for the rotor vanes = 12 nos. ($\theta=30^\circ$), 10 nos. ($\theta= 36^\circ$), and 8 nos. ($\theta= 45^\circ$), 6 nos. ($\theta=60^\circ$), and 4 nos. ($\theta= 90^\circ$), are increasing parabolically at rotor / casing ratios = 0.95, 0.90, 0.85, 0.80, 0.75 and 0.70 and it almost varies at different power values. It is also noticed that for the rotor vanes 6 nos. ($\theta=60^\circ$), and 4 nos. ($\theta= 90^\circ$) the values of power are found large.

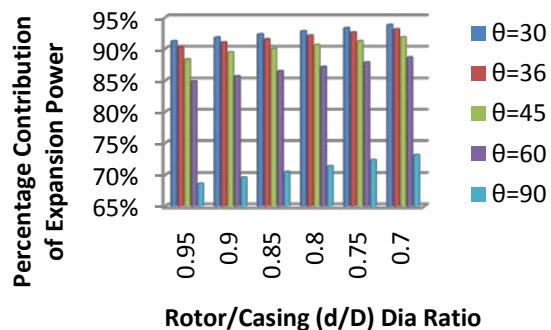


Fig.6 : Percentage contribution of expansion power versus rotor / casing diameter (d/D) ratio at different vane number (vane angles) when $D=100$ mm, injection pressure = 6 bar and speed of rotation = 2500 rpm

Figure 6 shows the percentage contribution of expansion power against total power output for different rotor / casing ratios = 0.95, 0.90, 0.85, 0.80, 0.75 and 0.70 at the rotor vanes = 12 nos. ($\theta=30^\circ$), 10 nos. ($\theta= 36^\circ$), and 8 nos. ($\theta= 45^\circ$), are increasing from 91-94%, 90-93% and 88-92% respectively. But at the rotor 6 nos. ($\theta=60^\circ$), and 4 nos. ($\theta= 90^\circ$), it varies from 85% to 87% and from 69% to 73% respectively.

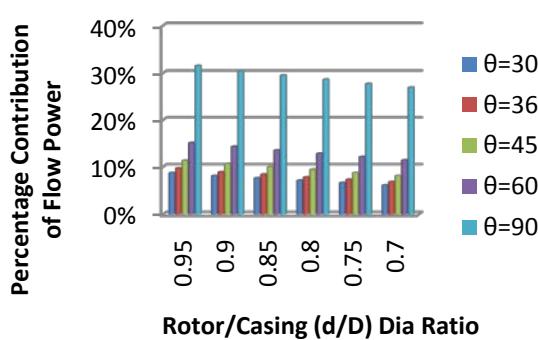


Fig.7: Percentage contribution of exit flow power versus rotor / casing diameter (d/D) ratio at different vane number (vane angles) when D=100 mm, injection pressure = 6 bar and speed of rotation =2500 rpm

Figure 7 shows the contribution of flow power against the total power output for different rotor / casing ratios =0.95, 0.90, 0.85, 0.80, 0.75 and 0.70 at the rotor vanes =12 nos. ($\theta=30^\circ$), 10 nos. ($\theta=36^\circ$), and 8 nos. ($\theta=45^\circ$) are decreasing from 11% to 6% and at the rotor 6 nos. ($\theta=60^\circ$), and 4 nos. ($\theta=90^\circ$), it varies from 15% to 11% and from 31% to 27% respectively.

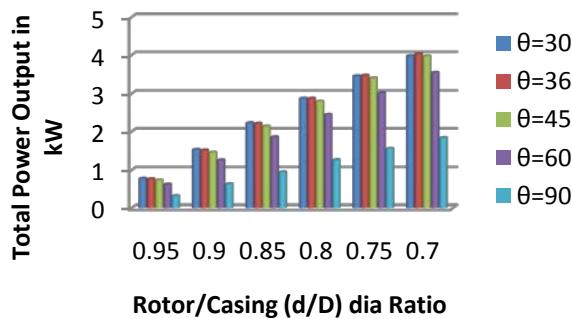


Fig.8: Total power output versus rotor/casing diameter (d/D) ratio at different vane angle when injection pressure = 6 bar and speed of rotation =2500 rpm

Variation of total power output is seen from Fig. 8, with respect to different vane angle = 30° (12 vanes), 36° (10 vanes), 45° (8 vanes), 60° (6 vanes) and 90° (4 vanes) are increasing linearly at rotor / casing ratios =0.95, 0.90, 0.85, 0.80, 0.75 to 0.70 and it almost varies in similar values. Thus optimal performance of total power is seen to be 4.02 kW at rotor / casing ratios =0.70 for vanes number 10 nos. ($\theta=36^\circ$). But variation of total power for the rotor vanes =6 nos. ($\theta=60^\circ$), and 4 nos. ($\theta=90^\circ$), are increasing linearly from rotor / casing ratios =0.95 to 0.75 and found smaller in its value than (d/D) =0.70.

From Fig. 8, a critical study is carried out and it is observed that the total power bar lines are almost equals at vane angle 30° - 36° (vanes= 12-10 nos.) for d/D ratios 0.90, 0.85, 0.80 and 0.75. The power output appears to be maximum when vane angle is 36° (vanes= 10 nos.) at d/D ratio=0.70. Accordingly a graph is drawn between "Total output power versus different vane angles" e.g., = 30° (12 vanes), 36° (10

vanes), 45° (8 vanes), 60° (6 vanes) and 90° (4 vanes) as shown in Fig. 9. It is thus observed that in the vane turbine total shaft power output is although the combined effect of the component of expansion power and exit flow power, but contribution of expansion power is predominant. The contribution of exit flow power due to steady flow in respect to total power output varies from 6.2% to 31.4% for injection pressure of 6 bar and speed of rotation at 2500 rpm.

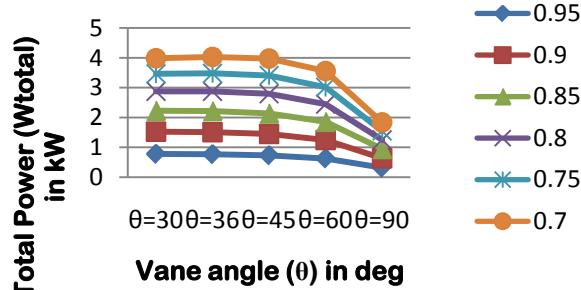


Fig.9: Total power output versus vane angles (vane numbers) at different rotor / casing (d/D) ratio when injection pressure = 6 bar and speed of rotation =2500 rpm

From Fig. 9, it is obvious that the expansion power output as well as total power output is found optimum when vane angle ranges from 30° - 45° (12-8 vane nos.), injection angle at 60° or above, at rotor/casing diameter ratio 0.70, speed of rotation at 2500 rpm and injection pressure at 6 bar and will be a deciding factor for desired shaft power output.

VI. CONCLUSIONS

From the above investigations based on input parameters, such as; injection pressure, injection angle and speed of rotation when kept 6 bar, 60° and 2500 rpm respectively, following conclusions are drawn:

- 3.98 kW to 4.02 kW, when rotor to casing diameter ratio is 0.70 and vane nos. 12-8 (vane angle 30° - 45°),
- 3.46 kW to 3.48 kW, when rotor to casing diameter ratio is kept 0.75 and vanes nos. 12-10 (vane angle 30° to 36°),
- 2.79 kW to 2.87 kW, when rotor to casing diameter ratio is kept 0.80 and vanes nos. 12-10 (vane angle 30° to 36°).

Thus optimum shaft power output of a novel vaned type air turbine is obtained when the design parameters for rotor diameter to casing diameter (d/D) ratios are kept between 0.75 to 0.70 and vanes nos. 12-10 (vane angle is of 30° to 36°) and plays an important role in designing the air turbine.

VII. NOMENCLATURE

d	diameter of rotor ($2r$) in meter
D	diameter of outer ($2R$) cylinder in meter
L	length of rotor having vanes in meter
n	no. of vanes = $(360/\theta)$
N	no. of revolution per minute
p	pressure in bar
p_1, v_1	pressure and volume respectively at which air strike the Turbine,
p_4, v_4	pressure and volume respectively at which maximum expansion of air takes place,
p_5	pressure at which turbine releases the air to atmosphere.
v	volume in cu-m
w	theoretical work output in Nm
W	theoretical power output (Nm/s)
X_{1i}	variable extended lengths of vane at point 1
X_{2i}	variable extended lengths of vane at point 2
bar	(1 / 1.0132) atmospheric pressure

Subscripts

$1, 2, 3, 4, 5$	subscripts – indicates the positions of vanes in casing
e, exp	expansion
f, flow	flow
t, total	total
min	minimum
max	maximum

Greek symbols

α	angle BOF
α_1	angle LOF ($=180-\phi$)
α_2	angle KOF ($=180-\theta-\phi$)
β	angle BAF
γ	1.4 for air
θ	angle between 2-vanes (BOH)
ϕ	angle at which compressed air enters into rotor through nozzle
ξ_d	eccentricity ($R-r$)

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Study on Algorithms of Graphic Element Recognition for Precise Vectorization of Industrial Computed Tomographic Image

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Abstract - Circle, line and circular arc are the common basic graphic elements in industrial computed tomography (ICT) image. The algorithm of recognizing such elements is the key to industrial CT image precise vectorization. An industrial CT image vectorization system has been studied, including different recognition methods for these elements. Firstly, based on facet model, the sub-pixel edge of an industrial CT image is extracted. Then, the circles are recognized by an improved algorithm based on probability of existence map, while the lines are recognized with the set intersection algorithm of fitting a straight line, and the circular arcs are recognized by the combination of the perpendicular bisector tracing algorithm and least squares function. Finally, the graphic element parameters are measured according to recognition results, and the drawing exchange file (DXF) is produced and transmitted into the computer aided design (CAD) system to be edited and consummated. The experimental results show that these methods are capable of recognizing graphic elements in industrial CT image with an excellent accuracy, besides, the absolute errors of circles are less than 0.1 mm, and the relative errors are less than 0.5%. It can satisfy the industrial CT vectorization requirements of higher precision, rapid speed and non-contact.

Keywords : *Computed tomography, facet model, edge detection, vectorization.*

GJCT Classification : I.4.9



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Fenglin Liu^a, Bing He^a, Bi Bi^b

Abstract - Circle, line and circular arc are the common basic graphic elements in industrial computed tomography (ICT) image. The algorithm of recognizing such elements is the key to industrial CT image precise vectorization. An industrial CT image vectorization system has been studied, including different recognition methods for these elements. Firstly, based on facet model, the sub-pixel edge of an industrial CT image is extracted. Then, the circles are recognized by an improved algorithm based on probability of existence map, while the lines are recognized with the set intersection algorithm of fitting a straight line, and the circular arcs are recognized by the combination of the perpendicular bisector tracing algorithm and least squares function. Finally, the graphic element parameters are measured according to recognition results, and the drawing exchange file (DXF) is produced and transmitted into the computer aided design (CAD) system to be edited and consummated. The experimental results show that these methods are capable of recognizing graphic elements in industrial CT image with an excellent accuracy, besides, the absolute errors of circles are less than 0.1 mm, and the relative errors are less than 0.5%. It can satisfy the industrial CT vectorization requirements of higher precision, rapid speed and non-contact.

Keywords : Computed tomography, facet model, edge detection, vectorization.

I. INTRODUCTION

There has been remarkable research achievement in developing and applying computerized tomography (CT) technology for medical and industrial applications, particularly in the industrial area, such as aerospace, aviation, military, machinery and automobile. Industrial CT is not only effective to detect the inner construction and flaws of an object, but also necessary to nondestructively measure the size of

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workpiece [1, 2]. However, the two dimensional slice images acquired by the 3rd generation ICT device can't be edited in the existing computer aided design (CAD) system. And most industrial CT images are the workpieces' dislocation images, which have many geometrical elements, such as lines, circular arcs and circles. Several conventional vectorization methods, applied in engineering drawings and maps, come with disadvantages, including noise sensitivity, computational complexity and low accuracy. These shortcomings make it difficult to accurately measure the size of workpieces' inner construction. In order to overcome these problems, in this paper we investigate methods of industrial CT images precise vectorization.

Since the research of image vectorization started in the early 1970s, numerous approaches have been developed [3, 4]. Broadly, these algorithms can be divided into several groups: thinning algorithm, contour tracking, Hough Transform (HT), dynamic window method and global recognition algorithm. The main advantage of thinning algorithm is that it holds a better reservation of image topology information, and its processing data points are decreased. Nevertheless, it is sensitive to noise. As a solution of this problem, the contour tracking method is provided. Its processing rate is high, and the impact of the air bubble and burr defects on the vectorization effect is reduced. However, the recognition accuracy is low since the vector image is discontinuous. In terms of accuracy and robustness, the HT and its variants have been successfully used in image vectorization. These methods are robust against outlier and occlusion, but computationally expensive. Dynamic window vectorization algorithm was proposed as a relatively novel method. A major advantage of this method presents at its high recognition accuracy to crossing point. Unfortunately, the window is changing continually, so the robustness is not enough. With the vectorization technology improving, some researchers have presented global recognition method. In process of vectorization, the line width can be obtained. Meanwhile, the corresponding tracking mode is adopted for reducing the impact of line fracture and missing data. But the accuracy of crossing point should be further improved.

In view of the disadvantages of the current image vectorization methods, the key contribution of this paper is to investigate a vectorization system for industrial CT image. In this system, the sub-pixel edge of an industrial CT image is extracted based on facet model. Its execution time is reduced significantly by removing invalid data points. Then, the circles, lines and circular arcs are recognized respectively with the corresponding recognition algorithms. These algorithms improve recognition accuracy. Also, in the process of recognition, the obtained elements parameters are dynamically saved in the corresponding linked lists. Hence, the required computation storage space is much cheaper than the previous methods.

II. SYSTEM OVERVIEW

In the process of industrial CT image vectorization, it is critical to detect edges in the image which is an important stage as the quantity and quality of edge data will affect greatly the vectorization performance of the system. The sub-pixel edge contour is extracted by the edge detection algorithm based on facet model, after the pre-processing as Gaussian filter, binarization. For this contour, the recognition algorithms of graphic elements are implemented. Firstly, determine whether the contour is a circle by calculating the center's probability. If it is a circle, the improved fast algorithm of circle detection based on probability of existence map is utilized to recognize it. The obtained circle parameters by the least squares function (LSF) are saved in the circle chained list. Reversely, if it is not a circle, the contour curve is fitted into many short line segments by adopting the improved set intersection algorithm of fitting a straight line. Then, merge the short line segments into the long line segments. Finally, the perpendicular bisector tracing algorithm is adopted to find the long line segments which can be fitted into circular arcs. And the merged circular arcs' parameters are derived from the least squares function. These parameters are saved in the circular arc linked list. Another long line segments' parameters are saved in the line linked list. After recognizing these elements, their parameters are outputted for vector graph. The system architecture is summarized in Fig. (1).

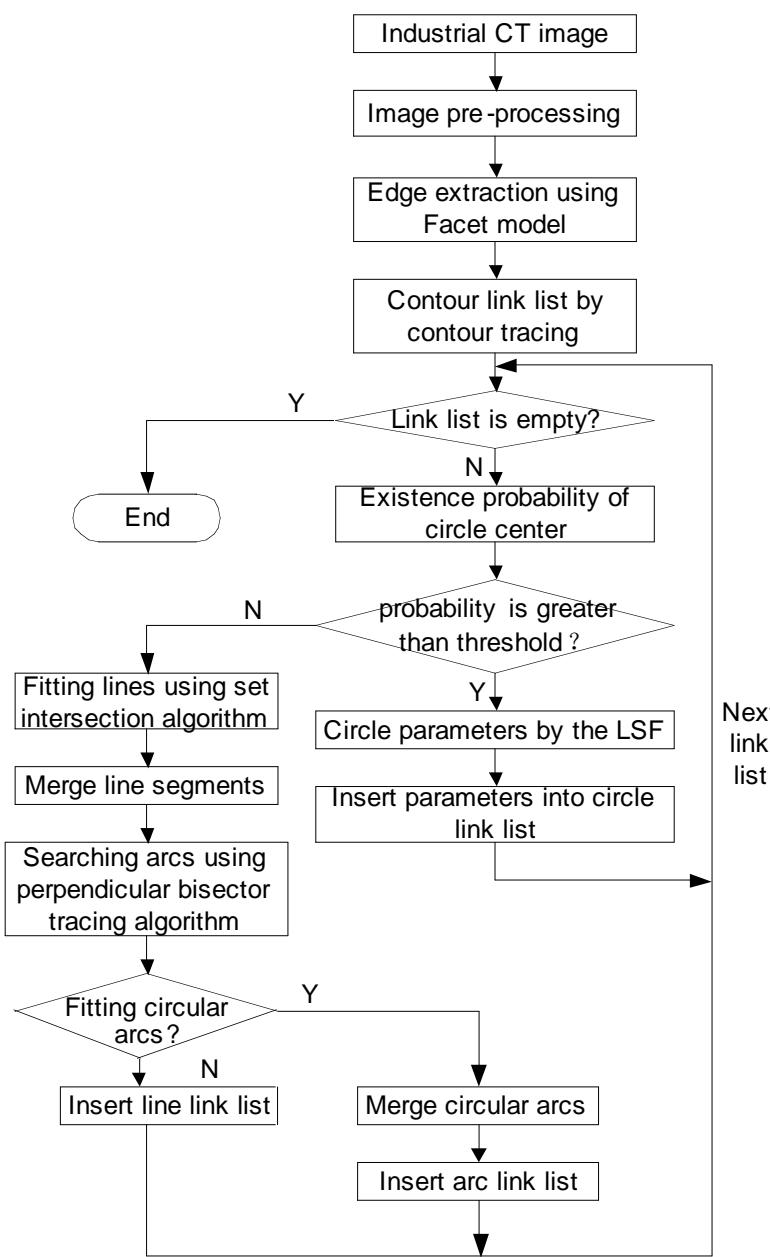


Fig. 1: Architecture of system.

III. EDGE DETECTING ALGORITHM BASED ON FACET MODEL

The exact location of edge is obtained by using the edge detection algorithm based on facet model. Through calculating the second-ordered directional derivative, edge point is defined as the zero-crossing point of facet model along the gray gradient direction [5]. Third-ordered facet model of the pixel (x, y) in 5×5 regions can be expressed as follows:

$$\begin{aligned} f(r, c) = & k_1 + k_2 r + k_3 c + k_4 r^2 + k_5 r c + k_6 c^2 + k_7 r^3 \\ & + k_8 r^2 c + k_9 r c^2 + k_{10} c^3 \end{aligned} \quad (1)$$

$r, c \in [-2, -1, 0, 1, 2]$.

Where (r, c) is the coordinate of any point in this pixel's neighborhood; $k_1 \sim k_{10}$ are the coefficients which are obtained by the least square method [6]. So

$$\sin \alpha = k_2 / \sqrt{k_2^2 + k_3^2}, \cos \alpha = k_3 / \sqrt{k_2^2 + k_3^2} \quad (2)$$

Define $r = \sqrt{\sin^2 \alpha + \cos^2 \alpha}$, $c = \tan \alpha$ (ρ is the distance between edge point and the center of pixel), the first-ordered, second-ordered and third-ordered partial derivatives of the model can be expressed as follows:

$$\left\{ \begin{array}{l} f'(\rho) = m_1 + 2m_2\rho + 3m_3\rho^2 \\ f''(\rho) = 2m_2 + 6m_3\rho \\ f'''(\rho) = 6m_3 \end{array} \right. \quad (3)$$

The edge point is the location of local extremum of the first-ordered derivative in local fitting surface; meanwhile it is the zero-crossing point of the second-ordered derivative as well. (r, c) is the edge point, if we can obtain ρ_0 (ρ_0 is within the 5×5 sub-region whose center is (r, c)) which satisfies (4), and the third-ordered partial derivative negative, as in (5).

$$f''(\rho) = 2m_2 + 6m_3\rho = 0 \Rightarrow |m_2/3m_3| = \rho_0 \quad (4)$$

$$f'''(\rho) < 0 \Rightarrow m_3 < 0 \quad (5)$$

Adopting this algorithm, the subtle image detail is located. The edge detection accuracy is high enough, and the image noise is restrained to some extent.

IV. RECOGNITION OF GRAPHIC ELEMENTS

a) Recognition of Circle

i. Existence Probability of Circle

Circles in the X-Y plane can be completely represented by the following quadratic equation with three parameters (u, v, r) as other 2nd order curves can be.

$$(x - u)^2 + (y - v)^2 = r^2 \quad (6)$$

In order to obtain the size and position of circles in industrial CT image, the method based on probability of existence map is applied [7]. P_e is the existence

probability of the circle whose center is (u, v) and radius is r . It is given by:

$$P_e = A(r) / 2\pi r \quad (7)$$

Where $A(r)$ is the amount of edge points, whose distance from the center equals r ; $2\pi r$ is the amount of discrete pixels of the circle with radius r .

Every pixel (x, y) in the image is regarded as the center, the existence probability P_e is calculated and saved in the two dimensional array $\{P(x, y)\}$. The probability of existence map is produced, and the radius r is saved in the two dimensional array $\{R(x, y)\}$. Each peak in probability of existence map represents that a circle may exist in this image, taking the peak coordinates as the center and r as the radius. P_e is the probability of such existence. Fig. (2) is an industrial CT image with a circle. The existence probability of the center point is calculated, and the probability map is shown in Fig. (3). The following information can be obtained : Center point (139,139), $r = 42.4946$, $P_e = 0.8996$

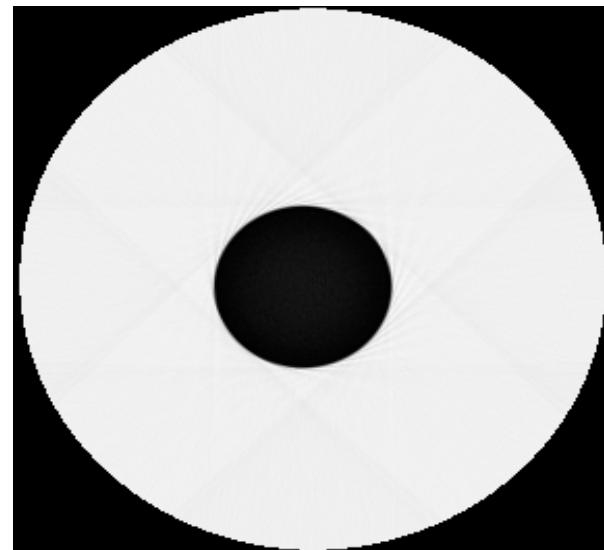


Fig. 2: Industrial CT image.

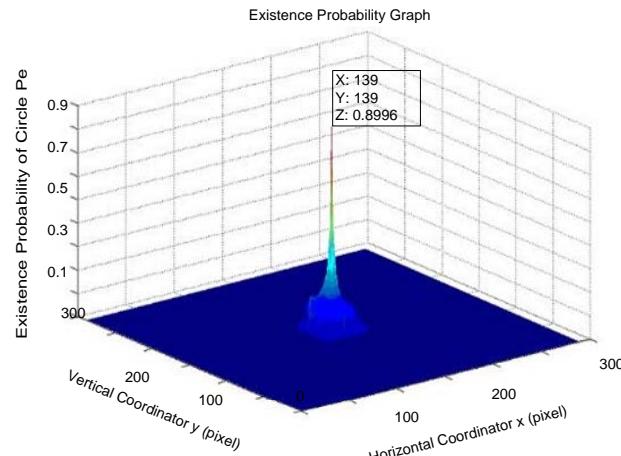


Fig. 3: Probability map of circle.

ii. *Improved Algorithm of Existence Probability*

The above algorithm regards each pixel in the image as the center of a circle, but most pixels in the image are not the center of the circle actually. As a result, the computation is complicated and the required computational storage is expensive. The center of the circle should lie in a mini-realm in the target region, thus, we improve the above algorithm by decreasing the select range of circle center to the square C [8]. If a closed curve has been recognized as a circle, the maximum distance of two points on the circle is defined as diameter, and the middle point of the diameter is the circle center. As illustrated in Fig. (4), for every closed contour, we first have to find the nethermost point A , then, calculate all distances from A to the other points. The point B that has the maximum distance D is the endpoint of the diameter. The midpoint O of the diameter is approximately regarded as the centroid of the closed contour. Therefore, a square C is obtained, whose center and sides are the centroid O and $D \times w$ ($D = 100$, $w = 0.1$), respectively. The square C is the area within which the potential circle center will be sought. In this way, the improved method constrains the search for potential circle center only in the specified small range and thereby reduces the computational cost.

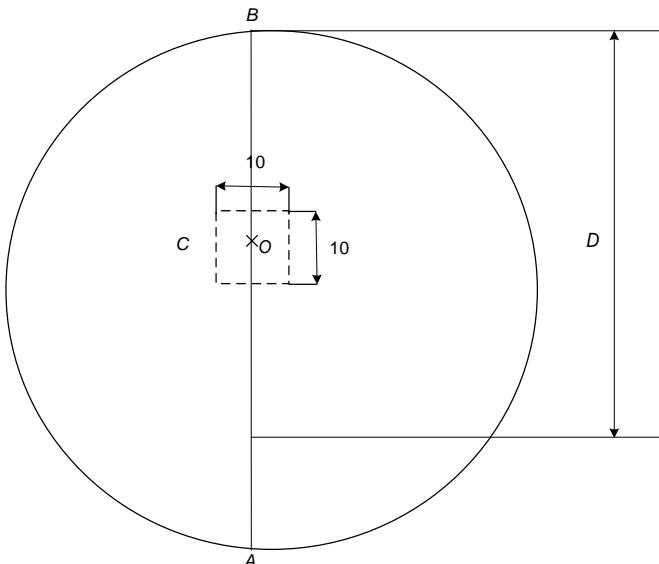


Fig. 4 : Select range of circle center.

Besides, we improved the storage mode for saving memory space as well. Circle parameters, such as the coordinates of the circle center, radius and existence probability, are stored by a series of two dimensional arrays in the previous algorithm, which has to allocate memory beforehand. Thus, different types of images require different memory size. If the allocated memory is oversize, the memory space will be wasted; on the contrary, if undersized, memory space will cause data overflow. In this paper, we store the above parameters using the chained-list, referred to as the

mode of allocating memory is dynamic, not beforehand. There is no need for this rule to redefine the memory size, even though the image size is different. As described in the following, the constructed list structure is effective in that it influences not only memory allocation, but also the recognition efficiency of a circle.

typedef struct

{int x; // x-coordinate of circle center
int y; // y-coordinate of circle center} Point;

struct NODE

{Point point; // coordinates of circle center
float r; // radius of circle
int k; // number of edge points
float p; // existence probability of circle
NODE *next; // the pointer of next node};

b) *Recognition of Line*

After recognizing the circles in industrial CT image, the remaining contours are fitted into short line segments by an improved method of fitting a straight line. Based on the set intersection algorithm of fitting a straight line [9], the method makes use of least square technique [10] to get line segment parameters. Generally, the procedure of the method is as follows:

As shown in Fig. (5a). For a contour, the starting point is P_0 , the current point is P_c . At the beginning of fitting, $P_c = P_0$. First, determine whether the next field of P_c is empty. If the next field is empty, end tracking the current line, get the line segment P_0P_c . If the next field isn't empty, judge whether the following point P_n belongs to the current line. If P_n is in the current line, then $P_n \rightarrow P_c$, and continue determining the following one. Or else, terminate tracking the current line, and get the line segment P_0P_c . Next, let P_n be the new starting point, and continue recognizing other line segments of the contour. After finishing a contour recognition, the above process is repeated for another contour of industrial CT image.

y_4			P_n		
y_3	P_0	P_c	■	■	
y_2	■	■			
y_1					
y_0					
	x_0	x_1	x_2	x_3	x_4

Fig.5(a) : Sketch map of straight line fitting

Due to low image quality and improper image preprocessing, the straight line may be mistaken as a series of short line segments, which we should merge into the long segments. The merging condition of two adjacent short line segments: the difference of slopes between two line segments must fall within the prescribed limits; and the distance between the endpoint of line segment and the merged long segment should be less than the specified value. As illustrated in Fig. (5b), if the angular difference between the adjacent line segments AB and CD is less than the prescribed value (using the angle value to represent the slope of line segment; here we choose 10°); and the distance from the point B to the line segment AC is less than the specified value (here 3 is appropriate), we will merge the short line segments AB and BC into the long segment AC . Then, determine whether the distance between the point C and the line segment AD is less than 3, and determine whether the angle difference between the line segment CD and the line segment AC is less than 10° . If the above two conditions are both met, get the long line segment AD . Or else, insert the merged line segment AC into the merged line link list, then, let CD be the new starting line segment, and continue merging the subsequent line segments.

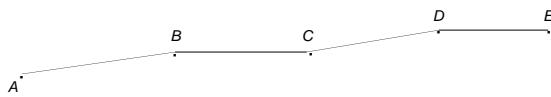


Fig. 5 (b) : Sketch map of merging line segment.

c) *Recognition of Circular Arc*

The obtained short line segments by implementing the above strategy are merged into the long line segments. These long line segments are fitted into circular arcs by means of the perpendicular bisector tracing algorithm [11]. The basic idea of the algorithm is that the perpendicular bisector of any chord on a circle passes through the circle center, and every endpoint of the chord is at an equal distance from the circle center.

As illustrated in Fig. (6a), any obtained line segment may be an approximation of an arc. We first consider the obtained line segment L_o as seed arc, its perpendicular bisector P_o is constructed. For every line segments L_i ($i = 1, 2 \dots N$), we then construct its perpendicular bisector P_i , and calculate the intersection C_i of P_i and P_o . Due to errors, the intersection C_i is not unique. However, all C_i are located along the line P_o . We define the point C_{\min} is the nearest point from L_o , and the point C_{\max} is the farthest point from L_o . Therefore, a rectangle C is obtained, whose length is the distance between C_{\min} and C_{\max} , and whose width is equal to the length of L_o and is bisected by P_o . The rectangle C is the area within which the potential arc center is sought.

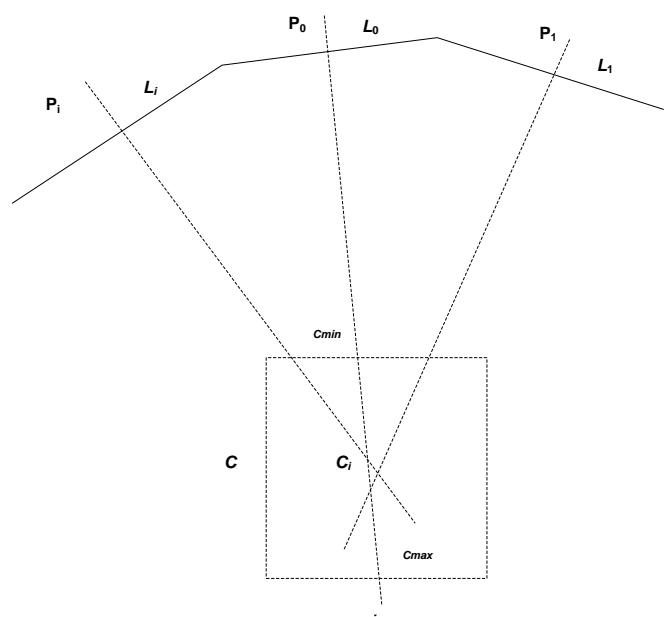


Fig. 6 (a) : Sketch map of circular arc fitting.

Having determined the potential center area, we check every pixel within it as a center candidate $c(x, y)$, the distances $R_i(x, y)$ between $c(x, y)$ and endpoints of line segments are gained. Then, we calculate the average radius $R(x, y)$ and the mean square error $ASD(x, y)$, using (8) and (9), respectively.

$$R(x, y) = \frac{1}{N+1} \sum_{i=0}^N R_i(x, y) \quad (8)$$

$$ASD(x, y) = \frac{1}{N+1} \sum_{i=0}^N (R(x, y) - R_i(x, y))^2 \quad (9)$$

The point whose $ASD(x, y)$ is minimal is taken as the circle center of circular arc, and the corresponding $R(x, y)$ is the radius of circular arc. The long circular arc may be recognized as some short circular arcs by using the perpendicular bisector tracing algorithm, so we merge these short circular arcs into the long circular arc. As shown in Fig. (6b), the merging condition of two adjacent short circular arcs: the coordinate difference between the circle centers O_1 and O_2 must fall within the prescribed limits (5 is fine); the radius difference between the radius R_1 and the radius R_2 should be less than the specified value (also 5 is enough); and the angular difference between the ending angle α_2 of the first circular arc and the starting angle α_3 of the second circular arc should be less than the threshold value (the threshold value is 3°). If there are two circular arcs meeting the above-mentioned three conditions, they can be merged into a new longer circular arc. The new circle center coordinates of this longer arc can be defined by the average value of the circle center coordinates of the two shorter arcs, and the

radius of this new longer arc can be replaced by the average value of the radius of the two shorter ones. Also, the starting angle and ending angle of this new arc are substituted with the starting angle α_1 of the first arc and the ending angle α_4 of the second arc, respectively.

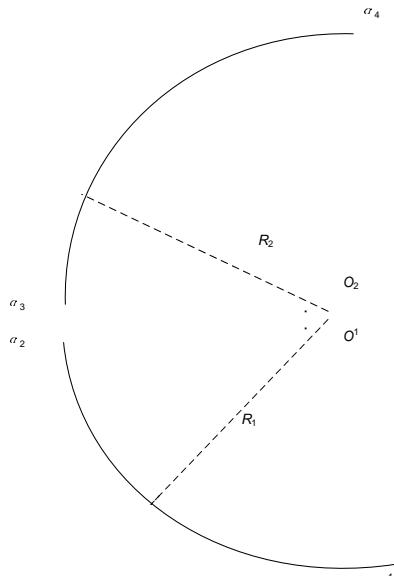


Fig. 6 (b) : Sketch map of merging circular arc.

V. EXPERIMENTAL RESULTS AND EVALUATION

a) Recognition of Circle

In this section, the performance of the proposed algorithms has been tested with the real industrial CT images. The algorithms are implemented in C++ with MS Visual C++ 6.0 compiler on a desktop PC with AMD 64 processor 1.81GHZ and 512MB RAM. The vectorization system for industrial CT image is designed, which provides the platform for our experiments. Fig. (7a) is an original industrial CT image of a socket set by the ICT system of CD-650BX in Chongqing University ICT Research Center. The technical indexes of the ICT system are as follows: the ray source is a 6/9MeV electron linear accelerator, the spatial resolution is 2.0lp/mm, the density resolution is better than 0.5%, the diameter of field of view is 398.872mm, the size of image is 800pixel*800pixel. Fig. (7b) is the sub-pixel edge image of circles in Fig. (7a); Fig. (7c) is the probability map of circles in Fig. (7a).

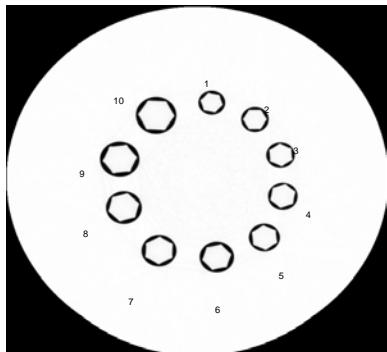


Fig. 7 (a) : Industrial CT image of a socket set

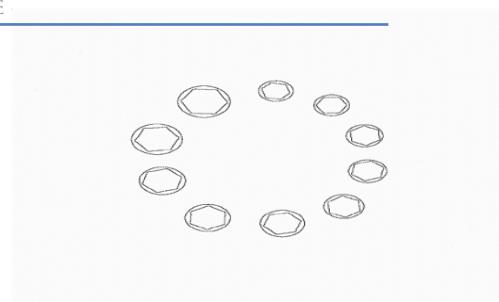


Fig. 7 (b) : Sub-pixel edge image

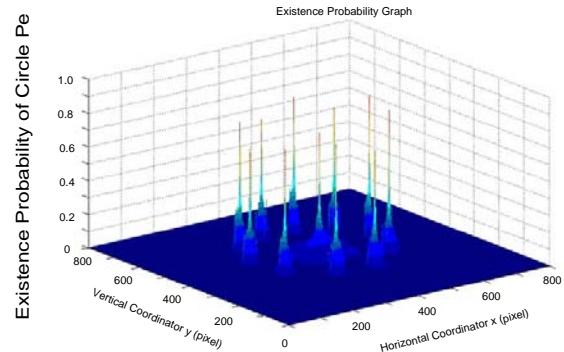


Fig. 7 (c) : Probability map of circles.

b) Measurement of Circle Parameters

The results of our algorithms on the industrial CT image of the socket set are summarized in Table 1. While in Table 2, we list the absolute error e between the true and measured values of a parameter, and we evaluate the relative error er as well. As can be seen from Table 2, our algorithms are able to achieve good accuracy. The absolute errors e of radius are less than 0.10mm, and the relative errors er are less than 0.5%.

Table 1 : Measurement Results of Circles

Number	Circle Center (pixel)	Radius (pixel)	Radius (mm)	P_e
1	(430, 576)	27.798	13.860	0.867
2	(520, 538)	28.452	14.186	0.919
3	(573, 455)	29.520	14.718	0.908
4	(578, 360)	30.635	15.274	0.774
5	(540, 264)	32.172	16.040	0.870
6	(440, 219)	35.642	17.770	0.785
7	(320, 233)	36.254	18.076	0.847
8	(246, 333)	37.170	18.533	0.729
9	(237, 445)	40.871	20.378	0.841
10	(314, 547)	42.133	21.007	0.877

Table 2 : Measurement Errors of Circles

Number	True Value (mm)	Measured Value (mm)	Error (mm)	Relative Error (%)
1	13.925	13.860	-0.065	0.467
2	14.240	14.186	-0.049	0.379
3	14.780	14.718	-0.062	0.419
4	15.350	15.274	-0.076	0.495
5	16.075	16.040	-0.035	0.218
6	17.810	17.770	-0.040	0.225
7	18.125	18.076	-0.049	0.270
8	18.590	18.533	-0.057	0.307
9	20.420	20.378	-0.042	0.206
10	21.230	21.007	-0.023	0.109

c) Vectorization Results of Whole industrial CT image

In addition, we evaluate the vectorization performance on two complicated images shown in Figs. (8a and 9a). Fig. (8a) displays an original industrial CT image of a car engine. Based on facet model, its edge image is extracted and shown in Fig. (8b). As seen from the edge image, the contour is clear and intact. Also, all small contours are extracted correctly. Fig. (8c) is the vector graph of the car engine by our algorithms; it is edited and perfected in AutoCAD2008. In this experiment, a threshold is set for determining whether the closed graphic element is circle. As observed in Fig. (8c), setting the threshold is 0.7, our algorithms not only detect these four large circles correctly, but also fit them with good accuracy. The sizes of circles are marked in AutoCAD2008. Nevertheless, the small circles and slight contours can't be detected completely. If we decrease the threshold value appropriately, these small circles and slight contours will be detected. But the vectorization accuracy may be dropped.

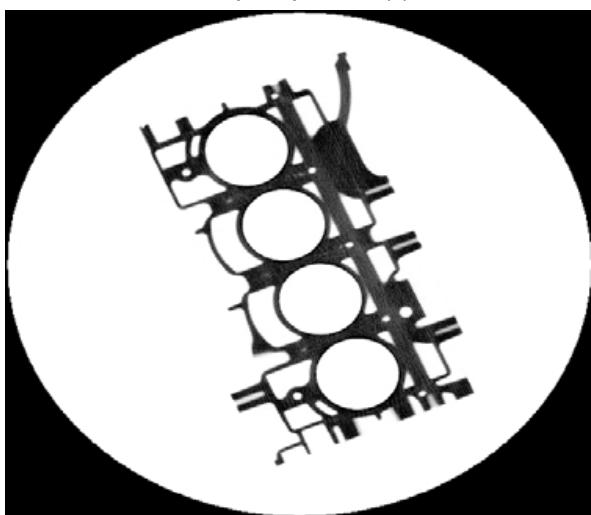


Fig.8 (a) : Industrial CT image of car engine

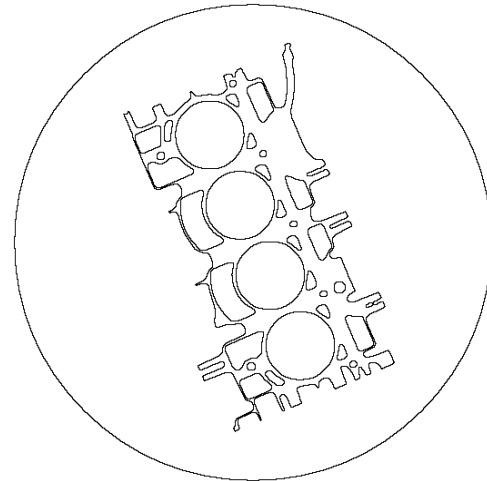


Fig. 8 (b) : Sub-pixel edge image of car engine

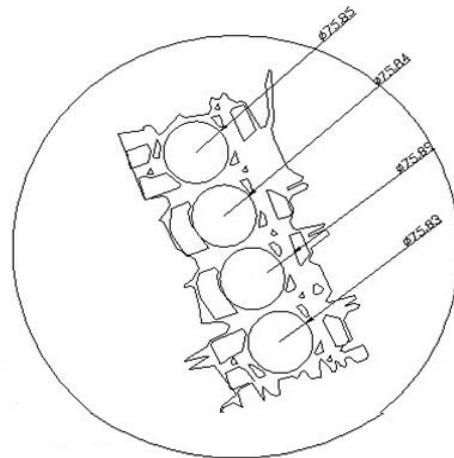


Fig. 8 (c) : Vector graph of car engine

Fig. (9a) shows an original industrial CT image of a gearbox cover. Unlike the previous industrial CT image of the car engine, this image has relative complex contours. In the top left corner are several small contours, which are difficult to be detected correctly. Despite this, its edge map is extracted completely and shown in Fig. (9b). Of particular interest is the vector graph of the gearbox cover in Fig. (9c) which evaluates our algorithms, and it is edited in AutoCAD2008. As shown in this picture, all circles are detected. Furthermore, several small circles are also detected and fitted correctly. Notice that the left isolated circle, which has the inner and outer concentric contours, is detected correctly. Also, the line contour can be fitted with ideal precision. However, Fig. (9c) also shows the limitation of our algorithms in the slight and complicated details of image. The circle with diameter of 16.55mm is nonexistent, it should not be found. And some contours are not with respect to the original contours ideally. For instance, the circular arc is represented by the irregular arc segments and curves. The following work will aim to resolve these problems.

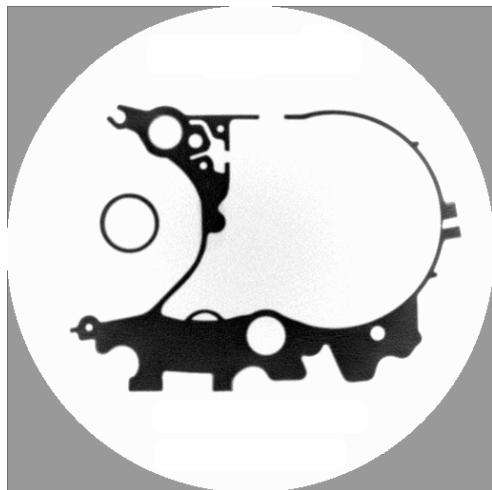


Fig. 9 (a): Industrial CT image of gear box cover

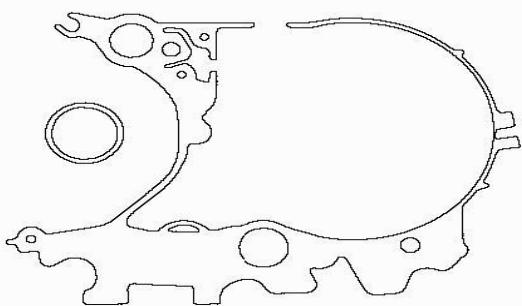


Fig. 9 (b): Industrial CT image of gear box cover

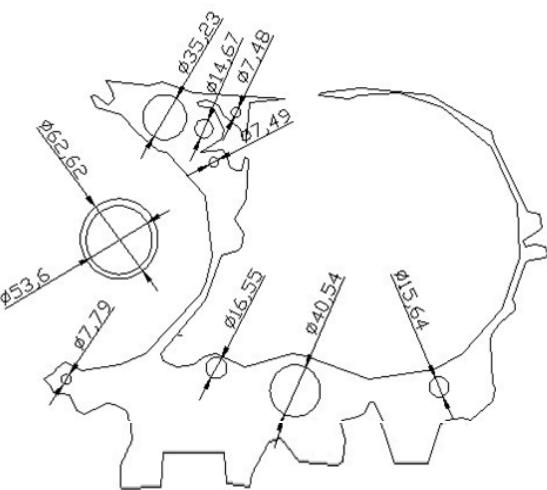


Fig. 9 (c): Industrial CT image of gear box cover

VI. CONCLUSIONS

In this paper, an algorithm for sub-pixel edge detecting based on facet model is adopted for the pre-processed industrial CT image. For the obtained contour, we can calculate the parameters of circle using the improved fast algorithm based on probability of existence map. Then, a set intersection algorithm of fitting a straight line is applied for recognizing the line. Finally, use the perpendicular bisector tracing algorithm and the least squares function to recognize circular arc. Thus, a vectorization system of industrial CT image is designed, which provides the platform for our experiments. Experimental results show indeed that our algorithms are capable of recognizing the circle, line and circular arc with an excellent accuracy. Furthermore, the vectorization performance for the whole image is preferable. It can satisfy the industrial CT image vectorization requirements of higher precision, rapid speed and non-contact. In the future, we will focus on extending this work by recognizing the relative complex graphic elements as ellipse, regular polygon.

VII. ACKNOWLEDGMENTS

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Numerical Computation of Economic Cooling Water rate for Two-stage Azeotropic Refrigerating systems

By D.V. Mahindru, Priyanka Mahendru

Abstract - With a view to conserve energy, the use of azeotropes in a multistage refrigerating system is quite timely. Depending upon the requirement, such a system incorporates conventionally either a water cooled or air cooled condenser. The total operating cost of a refrigerating system with a water cooled condenser comprises the cost of water and the cost of electricity needed to drive the compressor(s). There is enough potential for research in finding out the ways to achieve maximum coefficient of performance and the least operating cost simultaneously for multi-stage azeotropic refrigerating system. However, to avoid overloading of sewage facilities and to comply with municipal codes for the use of water, the water flow rate required in refrigerating system should be minimized.

In the present investigation, economic water rates for two stage refrigerating systems, operating on most commonly used azeotropes R-500 and R-502, have been searched out over a wide range of operating limits. Such economic rates, if followed, would produce maximum COP and consume minimum power. The effects of controlling variables, e.g. approach, cost ratio etc have also been studied on the heat transfer to condenser, optimum condensing temperature and economic water rate. The results have been presented in tabular form only.

Keywords : Azeotropes ,Multi – Stage , Refrigeration , Condenser, Thermodynamic Concept.

GJRE- C Classification : FOR Code: 091307, 091502



Strictly as per the compliance and regulations of:



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D.V. Mahindru^a, Priyanka Mahendru^Q

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I. DESCRIPTION

The total cost of a multistage refrigerating system with water cooled condenser comprises the cost of power required to run the compressors and the cost of water needed in the condensing unit to make the system work in a closed and continuous cycle. To minimize the total operating cost, the power consumed by compressors may be reduced by properly selecting their compression ratio, while cost on water can be diminished by consuming cooling water as low as possible. The compression ratio of a compressor gets affected, if either the condensing pressure or inter-stage pressure is changed. The quality of cooling water gets controlled by the quantity of heat to be transferred to the condenser. It is evident that larger is the water flow rate through a condenser, the lower will be the condensing temperature resulting in lower compression ratio for high pressure (HP) compressor and hence lower cost for

compressor power, but more cost on water. To the contrary, if the lower quantity of water is used, condensing temperature would be higher and thereby expenditure on water decreases while that on compressor power increases. Hence it calls for a compromise between condensing temperature and cooling water rate to achieve minimum total operating cost. The cooling water rate that minimizes the total operating cost is usually termed as *Economical Cooling Water Rate*.

II. REVIEW OF PREVIOUS WORK

To cope with the existing energy shortages and the need to conserve the expended energy to the maximum possible extent, attempts have been made by Macharnen and Chapman (4) and Downing (5) on various refrigerants and their mixtures. Among the mixtures of refrigerants, R-500 and R-502 have become very common. These are known as azeotropes. An azeotrope, by definition, is the mixture of refrigerants that does not separate into their original components with pressure/temperature changes. It has fixed thermodynamic properties unlike those of their components.

Azeotrope R-500 consists of 73.8% R-12 and 26.2% R-152. Its normal boiling point is about 3.5°C lower than that of R-12. It produces refrigerating effect per unit of swept volume about 18% more than that of R-12. A Freon-12 system designed for 60 cycle current can be shifted to 50 cycle current by using azeotrope R-500. It would result in approximately the same refrigerating capacity and evaporator and condenser conditions.

Azeotrope R-502 is a mixture of 48.8% refrigerant R22 and 51.2% refrigerant R-115. It boils at a temperature of about 4.8°C lower than that of R-22. Significantly lower discharge temperatures and lower winding temperatures are realized because of the higher capacities and lower values of compression ratio associated with R-502. Further R-502 decreases the swelling or softening effect on the common electrical insulating materials caused by the presence of R-115. The inter-stage pressure for the two stage refrigerating system is conventionally selected as the geometric mean of operating pressure limits to minimize the total compression work. But it has been established

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in (6) that if power input to the system is to be minimized, the inter-stage pressure should be optimized with coefficient of performance (COP) as the objective function.

III. THERMO DYNAMIC CONCEPT

In general, one may write the heat rejected to condenser for a refrigerating system as :

$$\dot{Q}_h = P(1+COP) \quad 1.1$$

But \dot{Q}_h per unit of cooling is expressed by :

$$\dot{Q}_h/\dot{Q}_c = P(1+COP)/\dot{Q}_c = (1+1/COP) \quad 1.2$$

Further, for a two stage refrigerating system, COP becomes maximum if inter-stage pressure is optimized for minimum power input. Equation 1.2 may be written as :

$$\dot{Q}_h/\dot{Q}_c = (1+1/COP) \quad 1.3$$

As $COP_o > COP$, We get

$$\dot{Q}_{ho} < \dot{Q}_h \text{ from equations 1.2 and 1.3}$$

"It means that heat rejection to condenser would be minimum and hence minimum quantity of cooling water would be required for given condenser when a two stage system operates with optimum inter-stage pressure/temperature as decided on the basis of minimum power input."

Thus the problem of finding out economical cooling water rate for a two stage refrigerating system is coupled optimization problem, that is, first the system needs to be optimized for its minimum power consumption, and then optimum condensing temperature is to be searched out to minimize the total operating cost.

IV. PRESENT WORK

In the present investigation, azeotropes R-500 and R-502 have been selected as the working fluids for two stage refrigerating system. Economic water rates that minimize the total operating cost and maximum COP are searched out over a wide range of operating temperature limits. Optimum design quantities of interest are presented in the form of tables. Effects of operating variables on the design quantities are also displayed through tables.

V. SYSTEM ANALYSIS

a) System Employing Water Cooled Condenser

Figure -1(a) shows the schematic of idealized two stage refrigeration system. The various heat and work quantities and pressure levels are indicated in the figure. The following simplifying assumptions are made for this system analysis :

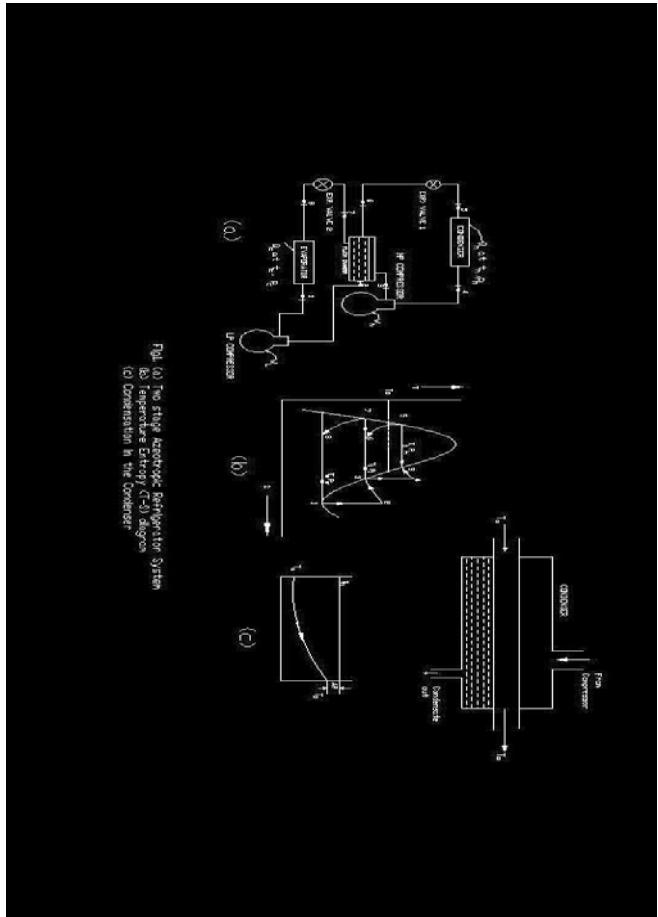
i. The thermodynamic cycle of the system is a standard one comprising isentropic compression, isentropic expansion and absence of superheating of

the suction vapour and sub cooling of the high pressure (HP) condensate.

ii. The pressure drop in evaporator, compressor valves, condenser piping etc are neglected.

iii. Entire condensation of HP gas inside the condenser takes place at a fixed temperature (T_h).

Referring to fig-1(b), one may write refrigerant mass flow through LP compressor on per ton-hour basis as :



By energy balance on the flash chamber, refrigerant mass flow through HP compressor turns out to be :

$$\dot{M}_3 = \dot{M}_1 (h_2 - h_1) / (h_3 - h_6) = 12,600 (h_2 - h_1) / (h_1 - h_5) (h - h_5) \quad 5.2a$$

If we consider that refrigerant mass flow through LP compressor is unit kg, then mass flow through HP compressor based on similar lines, would be :

$$\dot{M}_3 = (h_2 - h_1) / (h_3 - h_6) \quad 5.2b$$

and, total compression work shall be :

$$W_T = (h_2 - h_1) + \dot{M}_3 ((h_4 - h_3)) \quad 5.3a$$

However, on the basis of per ton hour, the total compression work may be written as :

$$W = W_1 + W_2 = \dot{M}_1 (h_2 - h_1) + \dot{M}_1 (h_4 - h_3) \quad 5.3b$$

power consumption of the system :

$$P = W / (3600) \quad 5.4$$

For preliminary design purposes, the enthalpies per unit mass of superheated vapour at points 2 and 4 can be approximately related to the enthalpies per unit mass of the saturated vapours at points 3 and 4, respectively as:

$$h_2 = h_3 + T_i (s_1 - s_3) \quad 5.5$$

$$h_4 = h_9 + T_h (s_3 - s_9) \quad 5.6$$

saturated properties of both the azeotropes are estimated from the correlations available in reference (10)

The coefficient of performance of system shall be :

$$COP = \dot{Q}_c / W = 12,600 / W \quad 5.7$$

Economic water rate expression as developed in ref (7,8) per unit ton of refrigeration, when total operating costs are minimized, is given by :

$$M_{we} = 15.45 (\dot{Q}_h \Delta P_c / cW)^{0.5} \quad 5.8$$

When \dot{Q}_h is heat rejection to condenser per ton per hour and is given as :

$$\dot{Q}_h = \dot{M} (h_4 - h_5) \quad 5.9$$

ΔP is the increase in power 'P' per degree rise in condensing temperature.

Optimum condensing temperature is expressed as :

$$T_{ho} = T_{wi} + DT_o \quad 5.10$$

$$\text{Where } DT_o = 0.1545 (\dot{Q}_h / P \cdot C_w \cdot C)^{0.5} + AP \quad 5.11$$

With AP as the approach, Fig 1(c) representing the end temperature difference.

It is evident that the expressions given in equation 5.4 and 5.7 to 5.9 can be expressed in temperature alone. An explicit expression has not been attempted at as it becomes extremely involved. Moreover, it serves no useful purpose because We can directly feed the above expressions in computer program to evaluate the objective function. The governing performance quantities in terms of operating parameters/variables can be expressed as:

$$P = P(T_i, T_h, T_e, T_{wi}, AP, \dot{Q}_c) \quad 5.12$$

$$\Delta P = P(T_h + 1, T_i, T_e, T_{wi}, AP, \dot{Q}_c) - P(T_h, T_i, T_e, T_{wi}, AP, \dot{Q}_c) \quad 5.13$$

$$\dot{Q}_h = \dot{Q}_c (T_h, T_i, T_e, T_{wi}, AP, \dot{Q}_c) \quad 5.14$$

$$\dot{M}_{we} = \dot{M}_{we} (T_h, T_i, T_e, T_{wi}, AP, Q_c, C_w) \quad 5.15$$

$$COP = (T_h, T_i, T_e, T_{wi}, AP, \dot{Q}_c) \quad 5.16$$

b) Objective Function And Optimization

For case 1, the objective function is the total operating cost together with the COP as given by equations (5.15) and (5.16) above. The total operating costs are to be minimized producing maximum COP as well. Since total operating costs have been minimized while deriving expressions for economic water rate (\dot{M}_{we}).from equations 5.15 and 5.16, it is clear that \dot{M}_{we}

and COP depend upon interstage and condensing temperatures (T_i and T_h) if other parameters are kept fixed. It leads to a two dimensional maximization problem with the two decision variables (T_i and T_h) subject to the constraints:

$$T_e < T_i < T_h \quad 5.17$$

And

$$T_h > T_{wi} + AP \quad 5.18$$

c) Solution Technique

To find T_{ho} , where total operating cost is minimum together with the optimum system performance, initially some convenient $T_h > T_a$ was assumed. With the help of this T_h and given values of evaporator temperature(T_e) subroutine maximises the COP and transfers required optimum quantities (\dot{M}_3 and P) to the main program. Now T_h is increased by unit degree and the above process is repeated. P is determined. \dot{Q}_h is found from equation 5.9 in the main program. Thereafter, DT_o is estimated from equation 5.11 to determine T_{ho} from equation 5.10. With this new value of T_{ho} , the above computations are repeated till two successive values of T_{ho} differ by $\pm 0.1\%$. Condensing temperature , thus predicted , is the required optimum condensing temperature (T_{ho}) because it produces minimum operating cost for maximum COP. Finally, at T_{ho} , \dot{M}_{we} is determined from equation 5.8, Fig 1.2(a) and 1.2(b).

Different ranges of various operating parameters considered for the azeotropic systems are based upon practical considerations and their commonly adopted values. They are as follows:

- a) Evaporator temperature : 5 to -50°C
- b) Ambient/Cooling Water Temperature : 15 to 75
- c) Approach Temperature : 2 to 5°C
- d) Cost ratio : 0.5 to 10

VI. RESULTS AND DISCUSSIONS

SYSTEM WITH WATER COOLED CONDENSER

Besides the direct use of Tables 6-1 to 6-3 for preliminary optimum design of the systems, they also exhibit the quantitative effects of operating variables on the design quantities for a specified set of operating parameters. Not only this, the feasible operating conditions can also be achieved with the help of the figures achieved. The approach (AP) has been kept at 3°C. For a fixed set of R_c , AP, t_a and t_e values, t_{ho} for $R-500$ is found to be slightly higher than that of $R-502$. On the other hand, economic water rate and heat rejection to condenser \dot{Q}_{ho} are seen to be higher in case of $R-502$ for given R_c (except equal to 10) .AP, t_a and t_e refer Tables 6.1 to 6.3, the detailed graphical presentation is available in reference-11 (page 27 to 44).

COP's of R-500 system is observed to be higher than that of R-502 systems (Ref. Tables 6.1 to 6.3)

Azeotrope		R-502						R-500					
t_a (°C)	t_e (°C)	t_{lo} (°C)	t_{ho} (°C)	\dot{M}_{we} (Kg/ton-h)	\dot{Q}_{ho} (KJ/ton-h)	COP_o	t_{lo} (°C)	t_{ho} (°C)	\dot{M}_{we} (Kg/ton-h)	\dot{Q}_{ho} (Kg/ton-h)	COP_o		
20	-50	-7.66	30.34	595.01	18,289.2	2.21	-12.25	31.13	527.79	18096.5	2.29		
	-40	-3.01	30.53	547.61	17,280.1	2.69	-3.38	30.95	512.50	17067.8	2.82		
	-30	1.73	30.73	506.17	16,392.8	3.32	1.46	31.11	477.37	16215.0	3.49		
	-20	6.55	30.93	469.5	15,602.9	4.20	6.27	31.27	446.45	15462.3	4.40		
40	-50	4.12	49.72	725.90	20,435.5	1.61	2.91	49.94	680.87	19808.5	1.75		
	-40	8.55	49.92	662.23	19,193.4	1.91	7.43	50.8	628.80	18663.4	2.08		
	-30	13.06	50.12	606.87	18,106.1	2.29	12.28	50.22	583.64	17663.9	2.49		
	20	17.56	50.33	558.34	17,143.3	2.77	16.95	50.36	544.00	16784.4	3.01		
60	-50	16.17	69.13	911.86	23,414.2	1.17	15.10	69.32	831.87	22028.1	1.34		
	-40	20.27	69.32	824.51	21,817.0	1.37	19.69	69.47	761.94	20659.7	1.56		
	-30	24.45	69.51	749.28	20,429.9	1.614	24.27	69.63	700.83	19458.9	1.84		
	-20	28.71	69.71	683.87	19,210.3	1.91	28.81	69.79	647.39	18404.9	2.17		

Table 6.2: Effect of approach on the optimum design quantities for two-stage azeotropic refrigerating system incorporating water cooled condenser
 Design Parameters : $R_c = 3.0$ $t_a = 30^\circ C$

Azeotrope		R-502						R-500					
AP (°C)	t_e (°C)	t_{lo} (°C)	t_{ho} (°C)	\dot{M}_{we} (Kg/ton-h)	\dot{Q}_{ho} (KJ/ton-h)	COP_o	t_{lo} (°C)	t_{ho} (°C)	\dot{M}_{we} (Kg/ton-h)	\dot{Q}_{ho} (Kg/ton-h)	COP_o		
2	-50	-2.44	39.10	645.29	19,184.6	1.91	2.57	40.29	527.79	18096.5	2.01		
	-40	2.10	39.30	591.51	18,081.3	2.30	2.02	40.57	512.50	17067.8	2.42		
	-30	6.72	39.50	544.63	17,113.0	2.79	6.83	40.74	477.37	16215.0	2.94		
	-20	11.43	39.71	503.26	16,252.9	3.45	11.63	40.91	446.45	15462.3	3.63		
4	-50	-1.32	41.03	658.27	19,397.3	1.85	-1.82	41.90	680.87	19808.5	1.97		
	-40	3.34	41.23	602.83	18,271.2	2.22	2.86	42.09	628.80	18663.4	2.37		
	-30	7.87	41.44	554.58	17,283.0	2.69	2.69	42.23	583.64	17663.9	2.88		
	-20	12.50	41.65	512.05	16,405.7	3.31	3.31	42.39	544.00	16784.4	3.54		
6	-50	-0.71	42.0	665.00	19,505.8	1.82	-1.41	42.72	831.87	22028.1	1.95		
	-40	3.86	42.20	608.76	18,367.9	2.18	3.30	42.89	761.94	20659.7	2.34		
	-30	8.50	42.41	559.74	17,359.5	2.64	8.14	43.03	700.83	19458.9	2.84		
	-20	13.03	42.62	516.64	16,483.5	3.24	12.85	42.7	647.39	18404.9	3.49		

VII. CONCLUSIONS

Azeotrope R _c	t _e (°C)	t _o (°C)	t _h (°C)	R-502			R-500		
				M _{we} (Kg/ton-h)	Q ^{h_o} (KJ/ton-h)	COP _o	t _o (°C)	t _h (°C)	M _{we} (Kg/ton-h)
0.5	-50	3.92	49.48	295.59	20,407.2	1.61	2.90	50.013	277.90
	-40	8.57	49.94	270.49	19,198.4	1.91	7.54	50.34	257.40
	-30	13.2	50.41	248.71	18,138.0	2.28	12.43	50.67	239.05
	-20	17.82	50.89	229.41	17,196.7	2.74	17.29	51.01	223.10
5.0	-50	-2.78	38.51	828.24	19,121.7	1.93	-2.96	39.62	679.22
	-40	1.73	38.67	759.07	18,020.7	2.32	1.62	39.87	617.21
	-30	6.42	38.83	698.75	17,054.8	2.83	6.42	40.02	572.77
	-20	11.00	38.99	645.65	16,196.9	3.50	11.2	40.17	534.11
10.0	-50	-3.75	36.92	1153.26	18,953.4	1.98	-4.83	36.49	1271.04
	-40	0.82	37.03	1057.20	17,865.8	2.39	0.11	36.82	1098.81
	-30	5.38	37.15	973.64	16,912.1	2.92	4.54	37.39	904.37
	-20	10.02	37.26	899.93	16,065.0	3.64	9.41	36.79	998.34

Table 6.3: Effect of Cost Ratio on the optimum design quantities for two-stage azeotropic refrigerating system incorporating water cooled condenser
Design Parameters : AP = 3.0 (°C) t_a = 30°C

- For a preliminary design of two stage azeotropic refrigerating system, the Tables 6-1 to 6-3 presented can directly be used.
- Economic water rate and heat transfer to condenser turns out to be relatively lower in case of R-500 for a given set of condenser, evaporator, ambient and approach temperatures and cost ratio.
- R-500 system produces comparatively higher COP than R-502 system for specified operating conditions.
- The effect of approach temperature is more pronounced on the economic water rate than the other quantities. It should be selected quite carefully.
- Though, the initial investment in case of R-500 system turns out to be more than R-502 system, it would get compensated over a small span of time because of lower operating cost of the R-500 system.

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VIII. NOMENCLATURE

AP : Approach °C

C_1 : Cost of Electricity (Rs/kw-h).

C_w : Cost of Water (Rs/k- litre).

COP_o : Maximum co-efficient of performance.

h_x : Enthalpy per unit mass at state condition 'x' (kJ/kg).

\dot{M}_1 : Refrigerant mass flow through LP compressor 9kg/ton-h).

\dot{M}_3 : Refrigerant mass flow through HP compressor (kg/ton-h).

\dot{M}_{we} : Economic water rate (kg/ton -h).

M_3 : Refrigerant mass flow through HP compressor per unit mass flow through Lp compressor(kg/kg).

P : Power 9kw/ton).

P_o : Minimum power (kw/ton).

ΔP : Power increase per ton per degree rise in condensing Temperature (kw/ton -°C).

P_h : Condensing pressure (bar).

P_e : Evaporating pressure (bar).

P_{io} : Optimum inter -stage pressure (bar).

\dot{Q}_h : Heat transfer to condenser (kJ/ton -h).

\dot{Q}_{ho} : Heat transfer to condenser pertaining to minimum operating cost and maximum COP (kJ/ton-h).

\dot{Q}_c : cooling effect per unit mass flow through LP compressor (kJ/kg).

r_1 : Compression ratio (P_{io}/P_e) of LP compressor.

r_2 : Compression ratio (P_h/P_{io}) of HP compressor.

R_c : Cost ratio (c/c_w).

s_x : Entropy per unit mass at state condition(kJ/kg-k).

t_a, T_a : Ambient temperature (°C,K).

t_{w1}, T_{w1} : Inlet water temperature (°C,K).

t_h, T_h : condensing temperature (°C,K).

t_e, T_e : evaporating temperature (°C,K).

t_{ho}, T_{ho} : Optimum condensing temperature(°C,K).

t_i, T_i : Interstage temperatures (°C,K).

t_o, T_o : Outlet water temperature (°C,K).

t_{io}, T_{io} : Optimum interstage temperature(°C,K).

V_1 : Minimum volume flow through LP compressor per unit mass flow through LP compressor (m³/kg).

V_3 : Minimum volume through HP compressor per unit mass flow through LP compressor(m³/kg).

W_1 : compression work of LP compressor (kJ/ton-h).

W_2 : compression work of HP compressor(kJ/ton-h).

W : Total compression work (kJ/ton-h).

W_T : Total compression work (kJ/ton-h).



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Dynamic Programming and Taguchi Method Optimization of Water-Treatment-Plant Design

By Khezri-S.M, Dadras-P, Dadvar-E

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Keywords : Optimization of water Treatment - Plants, Process Optimization -Taguchi Design of Experiments.

GJRE - A Classification : FOR Code: 030301, 090401



DYNAMIC PROGRAMMING AND TAGUCHI METHOD OPTIMIZATION OF WATER-TREATMENT-PLANT DESIGN

Strictly as per the compliance and regulations of:



Dynamic Programming and Taguchi Method Optimization of Water-Treatment-Plant Design

Khezri-S.M^a, Dadras-P^Q, Dadvar-E^B

Abstract - System and process optimization are both necessary for overall system design in system optimization models, the objective is to determine the optimal system configuration while assuming the design and operating parameters of each individual process. In process optimization models the objective is to find the design and operating parameters of individual processes. The major disadvantages of GP and NLP algorithms are that global optima is not assured and they can not be directly used for system optimization because of the presence of discrete decision variables and required high computer storage [Dharmappa 1994] [Desmond F. Lawler. 2005] Using DP solely for large problems requires very high computer time for Data Processing [Mhaisalkar 1993]. The model of this research is DP model that employs Taguchi Experimental Design Method, whereupon the time of model analysis has reduced considerably. . Case study showed the capability of model in savings of roughly 9.5% in capital and annualized costs, compared to the conventional design besides the software has capability to performing sensitivity analysis and showing interactions between various Decision variables.

Keywords: Optimization of water Treatment- Plants, Process Optimization- Taguchi Design of Experiments.

I. INTRODUCTION

The water Industry is one of the principal industries in every country. The total expenditure for water supply, including operation and maintenance, accounts to nearly 6 billion dollars per year in the U.S alone, of this approximately 15% is spent on actual water treatment (Wiesner, 1985). This massive investment requirement calls for more economical system design to allow for an efficient use of public funds. This objective can be achieved using "Optimization". Because in many cases pilot scale studies are conducted prior to full-scale plant construction, the use of an optimization model can greatly reduce the time and money spent on the pilot scale study.

A water treatment system is a combination of several unit processes. Design of such a system is a

difficult task and the least cost design is most difficult of all. The principal unit process in a conventional water-treatment system includes coagulation-flocculation, sedimentation, filtration and disinfection. The performance of each treatment unit affects the efficacy of the subsequent units. Ideally, therefore, the design decisions should be made with regard to the interaction between various unit operations. So for very few works have been done on the optimization of a water treatment system. Letterman & Iyer (1977) analyzed the effects of selected process decision variables on overall system cost and performance. The authors used simplified process models (mostly empirical relationships). One comprehensive work is that of Wiesner et. al(1978)which is an important step towards the optimal design of water treatment system. The authors have provided a number of optimization models for integral analysis and economic optimization of the components of a water treatment plant. Mhiasalkar(1993) has developed a mathematical model incorporating the Performance relationships and cost functions for the component units of conventional water treatment system, and an algorithm using dynamic programming has described by them for functional and minimal cost design of the system. The last and one of the comprehensive models in this ground belongs to Dharmappa et. al (1994). The authors believe the incorporation of particle size distribution (PSD) is necessary for optimal process design and selection. In this context this works includes not only all three levels of system design but also process design and selection using PSD and the Algorithm they have used was a GP and NLP programming.

The major disadvantages of GP and NLP algorithms are that, global optima is not assured and they can not be directly used for system optimization because of the presence of discrete decision variables and requirement high computer storage. Using Dynamic Programming solely for large problems requires very high computer storage. Accordingly, this paper addresses it self to the development of a model for minimal cost and Energy design of a conventional water treatment plant using dynamic programming and Taguchi Design Of Experiments methods optimization model. The scope of this research was restricted to the economic optimization of conventional water treatment system for turbidity removal comprising four water treatment processes, which are listed in table 1.

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Table 1: Conventional water treatment processes considered in this study

1. Rapid Mixing (back Mix)
2. Flocculation (Horizontal)
3. Sedimentation (Rectangular)
4. Granular filtration (Downflow & constant Rate)

(Note: Specific type considered is given in parenthesis)

The serial and interactive nature of the various unit processes favors application of Dynamic Programming for minimal cost design. Dynamic Programming is a mathematical technique often useful for making a sequence of interrelated decisions. It provides a systematic procedure for determining the combination of decisions that maximizes overall effectiveness [Hillier 1967]. Deterministic dynamic programming can be described diagrammatically, as shown in Fig. 1

**Fig.1:** The basics structure for deterministic dynamic programming.

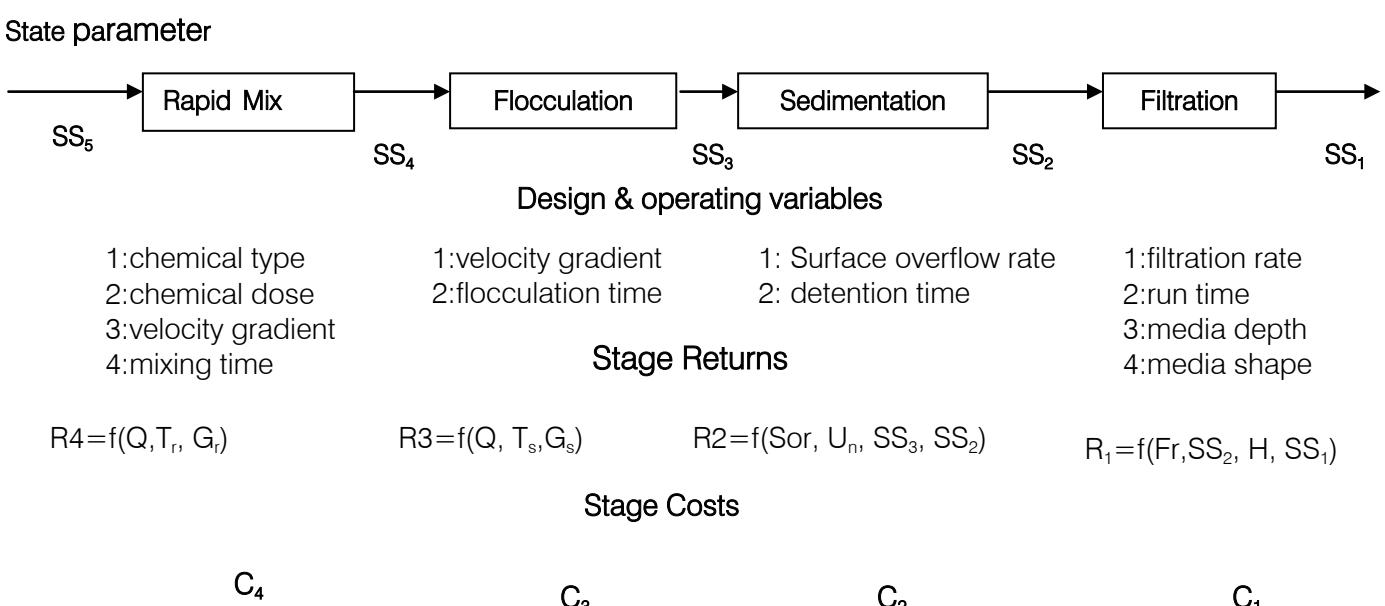
Thus at stage n the process will be in some state S_n . Making policy decision X_n then moves the process to some state S_{n+1} at stage $(n+1)$. From that point onward the objective function value for the optimal policy has been previously calculated to be $f^*_{n+1}(S_{n+1})$. Conventional water Treatment systems can be considered as a multistage process, with the stages

represented by various unit processes. The states represented by the levels of water quality parameters such as turbidity and suspended solids. The decision variables are design parameters depending on the type of unit.

Traditionally, measuring nonspecific parameters like turbidity units (Tu) suspended solids (SS); etc assesses the performance of water treatment plants. Though their parameters describe the important aspects regarding the water quality of the effluent from the treatment processes (AWWA: water 1990). Insofar as turbidity is used as a measure of the efficiency of the removal of particulate matter throughout the purification process of water, low turbidity in the finished water is an indication of effectiveness of unit processes (Guidelines 1984). Because mathematical models of water treatment describe the behavior of systems in relation to the removal of mass concentration of suspended solids. And we can in some ways correlate turbidity measurements with suspended solids data, suspended solids has been used as a state parameter to indicate the effectiveness of the system at various stages of treatment. Fig. 2 Show the sequence of stages and the stage return for each input-decision combination.

II. TAGUCHI METHOD

Taguchi approach to parameter design provides the design engineer with a systematic and efficient method for determining near optimum design parameters for performance and cost (Kackar, 1985; phadke, 1989; Taguchi, 1986). In this research we have used orthogonal arrays from design of Experiments theory to study a large number of variables with a Small number of experiments. Whereupon the time of DP model analysis reduced considerably.

**Fig.2 :** Unit sequences & Return of Conventional Water Treatment system

a) *Functional relationships of units*

Functional relationships for each unit process, linking input and output states parameters with a characteristic loading parameter, have been established based on the mechanics of unit process. These relationships are largely empirical models. Table 2 shows these relationships and key assumptions for each of the process models.

III. COST FUNCTIONS

Since the present study seeks to incorporate multiple design criteria in the optimization, there are three design criteria to be evaluated from the cost functions:

1. Annualized Capital Cost (ACC)
2. Operation & Maintenance cost (O & M)
3. Energy requirement (ER)

There is a substantial literature on cost functions for water treatment plant component (Hinomoto, 1977; Clark, 1982). The annualized capital and operation and maintenance cost functions are most taken from Clark (1982). Some changes have been made by Dharmappa (1994) so as to make them more general. Capital cost functions as presented by Clark (1982) were based on the annualization factor 0.102 (interest 8% and amortization 20 years). There were modified to incorporate a general annualization factor, of, which can be calculated by (assuming zero salvage value):

$$a_f = \left(\frac{i(1+i)^n}{(1+i)^n - 1} \right)$$

Where a_f = annualization factor;
 i = interest rate, Fraction; and
 n = amortization period, years.

Table 2: Relationships and keys Assumption for each of the process models.

		Functional Relationships Unit processes
Unit	Process	Relationships
Rapid Mix		$SS_5 + K \cdot A = SS_4$ A : alum dose K : Constant
Flocculation		$SS_4 = SS_3$ $d_f = 26.88 G_s^{-0.91}$ $T_s G_s^{2.8} = \frac{44 \times 10^5}{A}$ Ts: detention time Gs: applied velocity gradient d _f : average diameter of the floc
Sedimentation		$V_s = \frac{g}{18} (S_s - 1) \frac{d_f^2}{v}$ $\frac{SS_3 - SS_2}{SS_3} = 1 - [1 + n \frac{V_s}{Q/A}]^{-1/n}$ Q/A: surface overflow rate n: coefficient basin performance Vs: surface overflow rate for ideal basin
Rapid sand filter		$\frac{SS_2 - SS_1}{SS_2} = P_c$ $Y = 0.725 \cdot Fr^{0.29} d^{0.62} t$ $R = \frac{4/55 \cdot d^{2/5} H}{Fr^{1/2} SS_2}$ $\log\left(\frac{U}{13/3L}\right) = -0.208 + 1.950 \log\left(\frac{Y}{(13/3L)^{1/2}}\right) - 0.645 \left[\log\left(\frac{Y}{(13/3L)^{1/2}}\right)\right]^2$ $\log\left(\frac{R}{13/3L}\right) = -3.250 + 1.013 \log\left(\frac{Y}{(13/3L)^{1/2}}\right) - 0.036 \left[\log\left(\frac{Y}{(13/3L)^{1/2}}\right)\right]^2$ $P_c = \sum_{j=0}^{(t/2-1)} \frac{e^{(-u/2)} (u/2)^j}{j!}$ SS ₁ : influent suspension concentration H: increase in head loss at the end of t d: diameter of sand grain t: filter run time Fr: filtration rate

The relationships for energy requirement are developed from Gumerman et al. (1979). Cost functions for unit processes (extracted and compiled from Clark, 1982, with Dharmappa (1994) modifications are listed in Table 3.

In this table PR; DHR, PPI are: Power cost, Direct Hourly wages Rate and Producer Price Index respectively.

Table 3 : Cost function for various unit processes

Unit processes	Annual Construction Cost(ACC) Operation and Maintenance Cost (O & M)
Rapid mix	$ACC = 0.08507(Q \times Tr)^{0.79} (CCI)^{0.988} (1.0007)^{Gr} (a_f)$ $OM = 1.56947(Q \times Tr)^{0.799} (PR)^{0.717} (DHR)^{0.181} (1.00251)^{Gr}$
Alum dry stock	$ACC = 0.0197(A \times Q)^{0.656} (CCI)^{0.994}$ $OM = 3.30366 \times 10^{-4} (A \times Q)^{0.849} (PR)^{0.1847} (PPI)^{0.0259} (DHR)^{0.743}$
Flocculation	$ACC = 642.48(Q \times Ts)^{0.6916} (CCI)^{0.992} (1.00383)^{Gs} (a_f)$ $OM = 0.040581(Q \times Ts)^{0.785} (PR)^{0.357} (PPI)^{0.399} (1.0081)^{Gs}$
Clarifier	$ACC = 1872.527(A_c)^{0.701} (CCI)^{0.993} (U_n)^{1.00047} (a_f)$ $OM = 53.487(A_c)^{0.969} (PPI)^{0.181} (DHR)^{0.756} (U_n)^{1.006}$
Filter structure	$ACC = 13317.11(A_f)^{0.671} (CCI)^{0.989} (a_f)$ $OM = 913.377(A_f)^{0.549} (PR)^{0.147} (PPI)^{0.183} (DHR)^{0.61}$
Filter Media(single)	$ACC = 71.3413(A_f)^{0.9336} (CCI)^{0.996} (a_f)$ $OM = 0$
Filter backwash	$ACC = 108.127(6.1A_f)^{0.59} (ACC)^{0.966} (a_f)$ $OM = 747.398(6.1A_f)^{0.65} (PR)^{0.543} (PPI)^{0.219} (DHR)^{0.137}$
Filter surface wash	$ACC = 568.4533(A_f)^{0.801} (CCI)^{0.982} (a_f)$ $OM = 204.732(A_f)^{0.7146} (PR)^{0.526} (DHR)^{0.315}$

IV. MODEL OPTIMIZATION

There are a number of designs that satisfy water quality standards. The objective, therefore, is to minimize the system cost satisfying all constraints. The bounds used in the optimizations are given in table 4. The general form of objective function is expressed as.

$$\text{Opt} \cdot \sum_{i=1}^4 [R_i]$$

Design variables

Where: R= Stage Returns

Table 4 : bounds on variables used in optimizations

Variable	Units	Symbol	Lower bound	Upper bound
Velocity Gradient	s ⁻¹	G _r	400	1000
Mixing Time	S	T _r	10	50
Velocity Gradient	s ⁻¹	G _s	20	70
Flocculation time	min	T _s	10	60
Settling Time	hr	T _c	2	4
Settling Efficiency	-	-	0	0.95
Surface Overflow Rate	M hr ⁻¹	SOR	0.9	2.0
Filter Area	m ²	A _f	1	∞
Filter run time	hr	T _f	8	100
Filtration Rate	hr ⁻¹	F _r	3	15
Backwash fraction	-	B	0	0.15
Time for backwash	Hr	T _b	0.33	0.33
Terminal head loss	m	H	0	2.5
Filtrate mass Concentration	mg/L	C _{max}	0	2
Clarifier effluent Concentration	mg/L	C _e	2	20

V. RECURSIVE EQUATIONS

For deriving Recursive equations it is necessary the Return functions for

Table 5 : Economic data used in Return function

Item	Value
Power(PR)	0.04\$/kWh
Labor Wage Rate(DHR)	11.00\$/hr
Construction Cost Index/100(CCI)	3.25
Producer Price Index/100(PPI)	2.44
Alum	140\$/tone
Polymer	400\$/ tone
Polymer demand	6*10 ⁻⁸ moles/m ² of particle
Polymer molecular weight	5*10 ⁴

each unit process be prepared with economic data. The values of parameters for determining Return functions that are used in the optimizations, as well as the

assumed chemical costs are listed in Table 5. The Return functions for all unit processes are given in table 6

Table 6 : Return Equations of different unit processes

Units	Return Equation of units
Sand Filter	$R_1 = 8636.59(A_f)^{671} + 4688.94(A_f)^{546} + 46.877(A_f)^{9336} + 293.847(A_f)^{59} + 2006.13(A_f)^{65} + 363.86(A_f)^{801} + 119.195(A_f)^{7146}$
Sedimentation Tank	$R_2 = 1223.52(A_c)^{701}(U_n)^{1.00047} + 599.165(A_c)^{469}(U_n)^{1.006}$
Flocculation	$R_3 = 1.45443(Q.T_s)^{6916}(1.00383)^{G_s} + 0.0345(Q.T_s)^{785}(1.0081)^{G_s}$
Alum feed & Rapid mix	$R_4 = .54067(Q.T_r)^{.79}(10007)^{G_r} + 0.3817(Q.T_r)^{.794}(1.00251)^{G_r} + 0.12662(A.Q)^{.656} + 0.00160934(A.Q)^{.849}$

Now by using these Return functions we can derive the Recursive equations for all of the unit processes. The general forms of recursive equations for unit processes are given in table 7.

Table 7: Recursive equations of different unit processes

Units	Recursive equations of Units
Filter	$f_1^*(SS_2) = \text{opt.}[R_1]$ A_f, Q
Sedimentation	$f_2^*(SS_3) = \text{opt.}[R_2 + f_1^*(SS_2)]$ A_c, Q, G_s
Flocculation	$f_3^*(SS_4) = \text{opt.}[R_3 + f_2^*(SS_3)]$ G_s, T_s, Q
Rapid mix	$f_4^*(SS_5) = \text{opt.}[R_4 + f_3^*(SS_4)]$ A, Q, G_s, T_r, G_r

VI. OPTIMIZATION ALGORITHM

The sequential structure of serial systems can be exploited to transform the N-decision, one-state problems. This is accomplished by the procedure called dynamic programming, due to Richard Bellman (1957). The DP algorithm for functional and minimal cost design of water treatment system was developed in this research. The major inputs required are the design data on flow; raw-water suspended-solids concentration; alum dose; water temperature; and effective size, uniformity coefficient, and depth of filter sand. Data on unit costs of excavation, plain and reinforced cement concrete, steel, filter sand and appurtenances are also necessary. Data on discount rate, and chemical costs are required for economic evaluation. The algorithm involves four stages in DP programming, and the optimal function of the previous stage is implemented in the next stage. In each stage in addition to the previous optimal function, the return function concerning to the current stage is also used to optimize the existing stage.

This procedure will be followed until the last stage. The solution of this system is computed by backward form. With this parametric solution of stages, we can derive the optimal objective function in a parametric form. This parametric form includes all design parameters of the water treatment system. This objective function could be optimized by appropriate software based on the Taguchi Design of Experiments again could be calculated.

VII. CASE STUDY

The application of the optimization algorithm is illustrated for a 6250-m³/hr conventional water treatment plant. The optimal results of this model have been compared with EPA traditional water Treatment plant. Design criteria and cost calculation of EPA conventional water treatment plant exists in EPA Documents Gumerman et al. (1979). The optimal design results in saving of 9.5% in capital and Annualized cost. The comparison is presented in table 8.

Table 8: Comparison of Total Annualized Cost with EPA and Model 6250 m³/hr

Water treatment Plant Items	EPA WaterTreatment Plant	Suggested Model Water Treatment Plant
Total Annualized Cost(\$)	1046570	955757
Reduction(%)	9.5	

VIII. SENSITIVITY ANALYSIS

One particularly important feature of this model is the ease with which a sensitivity analysis can be carried out. This technique analyzes the sensitivity of the optimal solution to changes in various decision variables without re-solving the problem for each new value. It is highly unlikely that cost data of sufficient accuracy will ever be available (Walski 1991). Therefore, variation in total Annualized cost was also studied. The results of this analysis have been presented in table 9.

Table 9 : Optimum cost versus 3 more sensitive variables.

Parameter	Change in parameter over base value(%)	Optimal Design Value					Change in total annualized cost (%)
		SS ₂	SS ₃	G _r	T _r	T _s	
Flow	+10	7.5	150	400	20	20	+6.8
	+20	7.5	150	400	20	20	+12.6
	-10	7.5	150	400	20	20	-7.5
	-20	7.5	150	400	20	20	-15.2
Alum dose	+10	7.5	150	400	20	20	+3.6
	+20	7.5	150	400	20	20	+7.1
	-10	7.5	150	400	20	20	-3.76
	-20	7.5	150	400	20	20	-7.9
Filter Headloss	+10	7.5	150	400	20	20	-1.5
	+20	7.5	150	400	20	20	-2.95
	-10	7.5	150	400	20	20	+1.6
	-20	7.5	150	400	20	20	+3.39

The results signifies the objective function is more sensitive to Design flow rate (Q), alum dose (A) and gravity sand filter head loss (H) respectively. If the design flow is varied in the range of $\pm 20\%$, the total annualized cost will vary +12.6% and 15.2 %

A practical approach to analyzing either uncertain or variable situation is to test the sensitive of the optimal design to variation in key system parameters.

IX. CONCLUSION

So far very few works have been done on the optimization of a water treatment system. The scope of this research was restricted to the economic optimization of conventional water treatment systems for turbidity removal, comprising four water treatment processes (viz.-rapid mix, flocculation, sedimentation, and rapid sand filters). Mathematical models describing the performance relationships and cost functions for component units of a conventional water-treatment system have been formulated. By combining these models, an algorithm using Dynamic programming and Taguchi Design of Experiments methods software was developed for functional and minimal design of the system. The proposed approach is tested with a case study. The conclusions are listed as follows:

- The computer times requirements for this model is very less than other similar model doing the same task.
- The optimal design results in savings of roughly 9.5% in capital and annualized cost compared to the conventional design.
- The sensitivity analysis results signifies the objective function is more sensitive to design flow rate (Q), alum dose (A) and gravity sand filter head loss (H), respectively.

Suspension characteristics such as particle size and distribution are of significance in the overall process of water treatment. There are some shortcomings in major requirements for the successful incorporation of

PSD in the process design and selection. (Dharmappa, 1994). Future research dynamic programming & Taguchi methods optimization of water treatment plant design may be directed to test the feasibility of considering PSD and molecular particle size distribution in water and further research in the field of software development with more levels for control factors.

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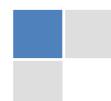
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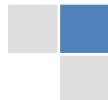
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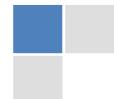
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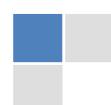
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All manuscripts submitted to Global Journals Inc. (US), ought to include:

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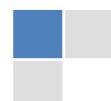
Key Words

A major linchpin in research work for the writing research paper is the keyword search, which one will employ to find both library and Internet resources.

One must be persistent and creative in using keywords. An effective keyword search requires a strategy and planning a list of possible keywords and phrases to try.

Search engines for most searches, use Boolean searching, which is somewhat different from Internet searches. The Boolean search uses "operators," words (and, or, not, and near) that enable you to expand or narrow your affords. Tips for research paper while preparing research paper are very helpful guideline of research paper.

Choice of key words is first tool of tips to write research paper. Research paper writing is an art. A few tips for deciding as strategically as possible about keyword search:



- One should start brainstorming lists of possible keywords before even begin searching. Think about the most important concepts related to research work. Ask, "What words would a source have to include to be truly valuable in research paper?" Then consider synonyms for the important words.
- It may take the discovery of only one relevant paper to let steer in the right keyword direction because in most databases, the keywords under which a research paper is abstracted are listed with the paper.
- One should avoid outdated words.

Keywords are the key that opens a door to research work sources. Keyword searching is an art in which researcher's skills are bound to improve with experience and time.

Numerical Methods: Numerical methods used should be clear and, where appropriate, supported by references.

Acknowledgements: *Please make these as concise as possible.*

References

References follow the Harvard scheme of referencing. References in the text should cite the authors' names followed by the time of their publication, unless there are three or more authors when simply the first author's name is quoted followed by et al. unpublished work has to only be cited where necessary, and only in the text. Copies of references in press in other journals have to be supplied with submitted typescripts. It is necessary that all citations and references be carefully checked before submission, as mistakes or omissions will cause delays.

References to information on the World Wide Web can be given, but only if the information is available without charge to readers on an official site. Wikipedia and Similar websites are not allowed where anyone can change the information. Authors will be asked to make available electronic copies of the cited information for inclusion on the Global Journals Inc. (US) homepage at the judgment of the Editorial Board.

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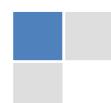
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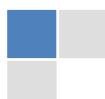
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- Submit to work done by specific persons (including you) in past tense.
- Submit to generally acknowledged facts and main beliefs in present tense.

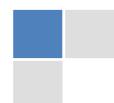
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	Containing all background details with clear goal and appropriate details, flow specification, no grammar and spelling mistake, well organized sentence and paragraph, reference cited	Unclear and confusing data, appropriate format, grammar and spelling errors with unorganized matter	Out of place depth and content, hazy format
<i>Introduction</i>	Clear and to the point with well arranged paragraph, precision and accuracy of facts and figures, well organized subheads	Difficult to comprehend with embarrassed text, too much explanation but completed	Incorrect and unorganized structure with hazy meaning
<i>Methods and Procedures</i>	Well organized, Clear and specific, Correct units with precision, correct data, well structuring of paragraph, no grammar and spelling mistake	Complete and embarrassed text, difficult to comprehend	Irregular format with wrong facts and figures
<i>Result</i>	Well organized, meaningful specification, sound conclusion, logical and concise explanation, highly structured paragraph reference cited	Wordy, unclear conclusion, spurious	Conclusion is not cited, unorganized, difficult to comprehend
<i>Discussion</i>	Complete and correct format, well organized	Beside the point, Incomplete	Wrong format and structuring
<i>References</i>			



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A 3D white figure stands at the bottom center, looking up at a large globe. The globe is mostly grey with a prominent green continent (representing South America) in the center. The figure has its arms raised, as if reaching for the globe.

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